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**EFFECT OF MATERIAL MASS DISTRIBUTION
ON THE LIFE OF SMALL ARMS BARRELS**

DARREL M. THOMSEN

APRIL 1976

FINAL REPORT

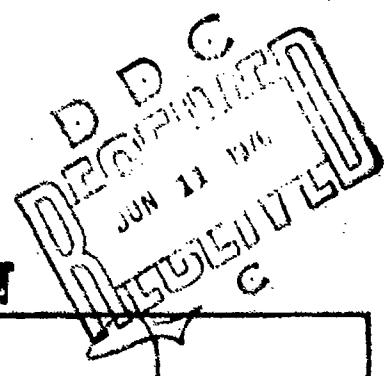
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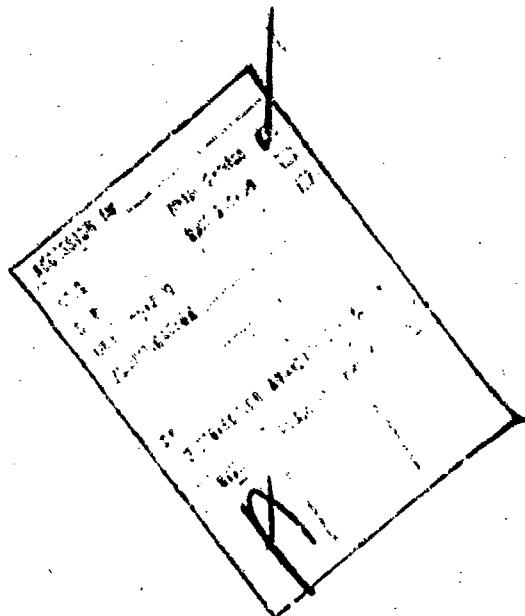
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This report covers FY75 efforts on a project entitled, "Effect of Material Mass Distribution on the Life of Small Arms Barrels." The objective of this project is to develop a semi-empirical technique for determining gun barrel wear (or erosion) as a function of barrel material properties, wall thickness (or ratio) and firing rate. The past years task involved analytical design of test specimens (barrel geometries) for firing experiments wherein regression analyses will be performed in the determination of the effect of mass distribution on barrel life. A useful design tool applicable in the optimum design

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of gun barrels was developed with the addition of a CALCOMP plot routine to an existing implicit finite difference computer solution. Examples of these plots are given as part of the results for the parametric barrel specimen design study.

CONTENTS

	<u>Page</u>
DD Form 1473	1
Contents	iii
Introduction	1
Analytical Approach	1
Results	4
Appendix 1	7
Appendix 2	12
Appendix 3	55
Distribution	S1

EFFECT OF MATERIAL MASS DISTRIBUTION ON THE LIFE OF SMALL ARMS BARRELS

INTRODUCTION

Much effort has been spent in the pursuit of meaningful gun barrel erosion analyses. Most of these efforts have dealt with specific mechanisms and consequently have comprised only fragmentary parts of the over-all erosion problem. It is commonly accepted that a more unified approach is required to accomplish comprehensive erosion research. Further, it is believed that an immediate need exists for empirical or semi-empirical techniques which predict erosion as a function of the basic parameters involved. Toward this objective, the task herein described was undertaken to define erosion in small arms gun barrels as a semi-empirical function of barrel mass, material properties and firing rate.

A report¹ published during FY74 entitled, "Small Arms Gun Barrel Thermal Experimental Correlation Studies," describes a correlation between muzzle end wall thickness and barrel life. As shown in Figure 1, rounds to failure based on firing accuracy measurements decreased from 10,000 rounds to 2,000 rounds as barrel wall thickness decreased from .461 inches to .125 inches. These efforts are a continuation of this work toward the stated objective of better quantifying the over-all erosion process.

ANALYTICAL APPROACH

Print-outs of the two computer programs utilized in this effort are contained in the appendixes. The first program (Appendix 1) calculates effective bore boundary conditions (propellant gas convection coefficients and temperatures) based on experimentally measured barrel temperatures. This solution utilizes an energy balance wherein the gun barrel performs as a mass type calorimeter. A complete

¹Report No. R-TR-74-034

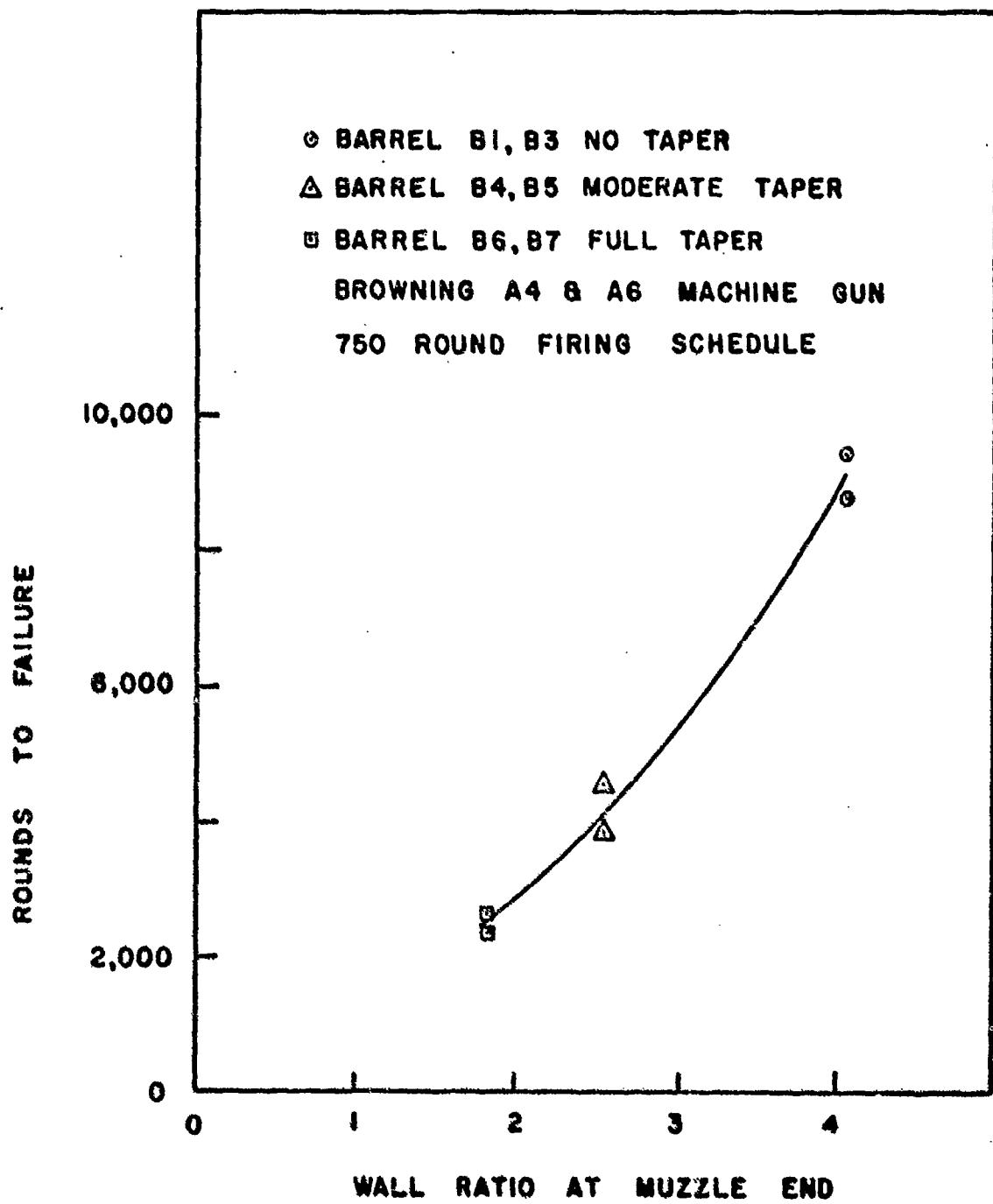


Figure 1 Geometry Effect on Barrel Life

description of this program is given in a report¹ entitled, "A Theoretical and Experimental Thermal Analysis To Determine Wall Ratios For A 30mm Tactical Barrel."

The second computer program (see Appendix 2) calculates transient gun barrel temperatures as a function of firing schedule and environmental conditions. This solution uses bore boundary conditions determined in the first program. The computer program employs an implicit finite-difference algorithm and continually performs an error analysis based on a numerical integrated energy balance. A major contribution to this effort was achieved by the incorporation of a plot routine capability. Computer graphics options which are available include:

1. Bore temperature versus firing time.
2. External barrel-temperature versus firing time.
3. Average radial temperature versus firing time.
4. Radial temperature distribution at prescribed times.

The main criteria used in selection of a test gun included; gun and ammo availability, ease of operation, and mechanism reliability. Based on these criteria, the Browning A4 was selected as a test vehicle. The over-all objective was to design axial barrel wall ratios such that the barrel would be subjected to uniform temperatures along the length of the barrel. A "gating" criterion was that of combined thermal pressure stresses. That is, the minimum thickness at any barrel section was designed of sufficient structural integrity to contain the propellant gas pressures. Consequently, subsequent to the heat transfer study, coupled thermal and pressure analyses were performed as the final design step. Once the minimum wall thickness barrel was designed, two larger barrels were designed where the wall thicknesses were arbitrarily increased in steps of .0625 inch. That is, the largest barrel has an outer diameter .250 inch larger at all axial locations than the minimum thickness barrel.

¹Report No. R-TR-75-023

The overall procedure applied in the design of the test barrels included the following steps:

1. Experimentally firing representative gun barrels to determine bore boundary conditions.
2. Calculating effective propellant gas temperatures and convection coefficients.
3. Parametric analyses wherein barrel temperatures were calculated for a fixed rate of fire and varying wall thicknesses.
4. Combined thermal pressure stress analyses to determine the minimum allowable barrel thickness as a function of the previously determined temperatures.

RESULTS

Results of the thermal analysis are given in Appendix 3. As previously stated the objective of this parametric study was to design gun barrels of various wall ratios to determine the effect of barrel mass on erosion. The design firing schedule was fixed at continuous burst of 400 rounds total at a firing rate of 600 rounds per minute. Results are presented at axial locations 5, 9, 15 and 21 inches from the breech end. The notes for each curve give effective convection coefficients and gas temperatures. A summary of the various wall thicknesses considered is shown in Table 1.

Shown in Table 2 is a summary of the results including calculated maximum bore pressure stresses and average barrel operating temperatures for the various outer radii. Also given is the dynamic yield strength temperature corresponding to the maximum calculated pressure stresses. The final criterion used in the design of the minimum wall ratio barrels was a maximum barrel operating temperature of 1400°F average. This criterion satisfies the yield strength requirement at all locations and is conservative at the 15 and 21 inch locations. A sketch showing the outer profiles of the minimum wall ratio test barrel is given in Figure 30 (Appendix 3). It is recommended that the two larger barrels be constructed with increasing wall thicknesses of 1/16 inch and 1/8 inch respectively at each axial location.

TABLE 1
Various Outer Radii Analyzed

Axial Location (Inches) & Figure Number (Appendix 3)							
Inches	Fig.	Inches	Fig.	Inches	Fig.	Inches	Fig.
5	2	9	10	15	18	21	22
↑	{ 3	↑	11	↑	19	↑	23
↓	{ 4	↓	12	↓	20	↓	24
5	5	13	14	15	21	21	25
↓	{ 6	↓	14	↓		↓	26
↓	{ 7	↓	15	↓		↓	27
5	8	16	17	↓		↓	28
↓	9	9	17	21		21	29

TABLE 2

Summary of Analytical Results
(See Appendix 3)

Axial Location From Breech End Inches	Outer Radius Inch	Max. Yield Stress PSI	Average Barrel Operating Temperature °F	Limiting Temperature °F Based on Dynamic Yield Strength of Cr-Mo-V Steel
5.0	.674	92,251	1222	1240
5.0	.612	93,545	1361	1400 (Data Pt.) 1230 (Curve)
5.0	.542	95,194	1516	1400 (Data Pt.) 1220 (Curve)
9.0	.450	71,133	1352	1420
9.0	.420	72,453	1438	1410
15.0	.450	45,673	1287	1600*
15.0	.420	46,521	1351	1600*
15.0	.400	47,218	1390	1600
15.0	.37	48,537	1438	1600*
15.0	.34	50,332	1473	1560
21.0	.40	31,350	1319	1600*
21.0	.34	33,418	1434	1600*
21.0	.31	35,111	1470	1600*
21.0	.28	37,666	1492	1600*
21.0	.25	41,874	1503	1600*
21.0	.22	49,680	1511	1570
21.0	.20	60,678	1516	1510

*Extrapolated

APPENDIX 1

4000.000000 0.500000 225.000000 0.2000 1.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000
0.0075 0.022449 0.110000 1050.000000

APPENDIX 2

```

//MKOL4801 JOB (2703,1140+5,4+999) //10. TRANSFER PLOT, PARM=PLT2A,PARMLIB=0. THREESIX,    JOB 897
// EXEC SIMPLOT, PLOTTER=PLT2C,MAXPLTS2A,PARMLIB=0. THREESIX,
// FORTN4150
K1SIMPLOT PROC SYSOUT=4,MAXPLTS2A,PLOTTER=PRINTER
      EXEC VMEFORT,REGION=100K,OPTRT=13+3;
      EXEC SYSOUT=4,SYSPRT=SYSPUT
IEF2371 SUBSTITUTION JCL /* SYSOUT=4
      DO USNAME=OBJECT,UNIT=DISK,SPACE=(CYL,(1,1))
      PCBSIZE=0,DISP=(PASS)
      /FORT,SYSSIN DD *
IEF2361 ALLOC,FCW=MKOL4801,FORT
IEF2371 CDD ALLOCATED TO SYSPRINT
IEF2371 145 ALLOCATED TO SYSLIN
IEF2371 090 ALLOCATED TO SYSTEM
IEF1421 - STEP WAS EXECUTED - CND CODE 0006
IEF2851 SYSPRT=SYSPUT,DISK=1135,AV0000.MKOL4801.OBJECT
IEF2851 VOL SER NOS5,OFSE3.
IEF3731 STEP /FORT / START 75094.1135 CPU 00:24:56 SEC MAIN 100K LCS 0K
IEF3741 STEP /FORT / STOP 75094.1137 CPU 00:24:56 SEC MAIN 100K LCS 0K
*****STEP FORT ****JOB MKOL4801 ****DISK(10) ****UNITS(U1) ****IM-KASP(10) ****OUT OTHER(10) ****CPU TIME(10) ****STEP TIME(10) ****
ERESOURCE- CORE(K) DISK(10) UNITS(U1) IM-KASP(10) OUT OTHER(10) CPU TIME(10) STEP TIME(10) 00:00:19.34 00:00:19.43
EUSAGE- 150 0 0 556 617 0
*****END STEP ****
      EXEC #GMEPIAOMA,PARMLIB=1,LET=NOREF,SCTR=,REGION=98K, C0000060
      COND=(LT,FORT,DISP=(13+3)) 00000070
      K1SYSPRINT DD SYSOUT=4,SYSPRT=SYSPUT 00000080
IEF2371 SUBSTITUTION JCL /* SYSOUT=4
      XKSYSLIN DD DSNAME=SYSLIN,FORTLIB=DISP=SMR 00000090
      XKSYSRSH DD DSNAME=PARSCH,SIMPLIB=FORTLIB,DISP=SMR 00000100
      XKSYSRSH DD DSNAME=OBJECT,DISP=(OLD,DELETE) 00000110
      XKSYSIN DD DSNAME=SYSIN 00000120
      XKSYSUT1 DD UNIT=DISK,SPACE=(CYL,(1,1)) 00000130
      XKSYSFLND DD DSNAME=LOAD(MAIN),UNIT=DISK,SPACE=(CYL,(1,5+1)) 00000140
      XKSYSFLND DD DISP=(PASS) 00000150
IEF2361 ALLOC,FCW=MKOL4801,LKED
IEF2371 090 ALLOCATED TO SYSPRINT
IEF2371 150 ALLOCATED TU SYSLIB
IEF2371 265 ALLOCATED TO SYSTEM
IEF2371 145 ALLOCATED TO SYSLIN
IEF2371 145 ALLOCATED TO SYSPRINT
IEF2371 145 ALLOCATED TO SYSLIB
IEF1421 - STEP WAS EXECUTED - CND CODE 0006
IEF2851 SYS1.FORTLIB
VOL SER NOS5,OFSE3.
IEF2851 SYSPRT=SYSPUT,DISK=1135,AV0000.MKOL4801.P0000004
IEF2851 VOL SER NOS5,OFSE3.
IEF2851 VOL SER NOS5,OFSE3.
IEF3731 STEP /LKED / START 75094.1137 CPU 00:24:56 SEC MAIN 98K LCS 0K
IEF3741 STEP /LKED / STOP 75094.1138 CPU 00:24:56 SEC MAIN 98K LCS 0K
*****STEP LKED ****JOB MKOL4801 ****DISK(10) ****UNITS(U1) ****IM-KASP(10) ****OUT OTHER(10) ****CPU TIME(10) ****STEP TIME(10) ****
ERESOURCE- CORE(K) DISK(10) UNITS(U1) IM-KASP(10) OUT OTHER(10) CPU TIME(10) STEP TIME(10) 00:00:01.79 00:00:01.63
EUSAGE- 150 0 0 0 0

```


IEF2851	SYS7504.1135.0700.WKULABG1.LNAD	DELETED
IEF2851	VOL SER NOSE DFSE 3.	DELETED
IEF2851	SYS7504.1135.0700.WKULABG1.SW	
IEF2851	VCL 51 NOSE DFSE 3.	
IEF3751	JOB /WKULABG1 START 75744.1135	
IEF3761	JOB /WKULABG1 STOP 75094.1141 CP:1 14IN 34.66SEC	
BU4751	BU4751-CORE (101) DISC(101) TAPE(101) MASPI(101) OTHER(101)	CPU(C) TOTAL
ECOSTS	\$0.05 10.1 50.00 40.00 30.00 <0.00 \$0.00	\$5.78 \$6.80

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PAGE 0001
MAIN          DATE = 75094   11/35/51

C ONE-DIMENSIONAL TRANSIENT HEAT CONDUCTION PROGRAM MFT-24,
C PROVIDED BY THE NAVY A.M.C.LAWSON INC. VERSION = 1 JULY 1970
C THIS PROGRAM IS A GENERAL PROGRAM FOR THE SOLUTION OF CONDUCTION
C PROBLEMS WITH UP TO LESS DEGREES INCLUDING INTERFACIAL RESISTANCES
C BETWEEN DIFFERENT DIMENSIONS AND MATERIALS.
C
C+DEFINITION OF LAYERED COMPLEX -- BLK1=BLK2, AND RLX3
C COMMON /RLX3/ RLX1,RLX2,C11501,RLX1(150),RLX2(150),RLX3
C COMMON /ADDFL1/ ADDFL1,ADDFL2,ADDFL3,ADDFL4,ADDFL5,ADDFL6
C 2HRL1(150),RLX155,RLX2,CP2,RLX2,RLX3,RLX4,RLX5,RLX6,UR(10),
C RLX7,RLX8,RLX9
C COMMON /RLX3/ RLX1500,RLX1501,RLX1502,RLX1503,RLX1504,RLX1505,
C RLX1506,RLX1507,RLX1508,RLX1509,RLX1510,RLX1511,RLX1512,RLX1513,
C RLX1514,RLX1515,RLX1516,RLX1517,RLX1518,RLX1519,RLX1520
C COMMON /RLX3/ RLX1521,RLX1522,RLX1523,JO,NSUP
C
C+INITIALIZATION OF VARIABLES NOT LOCATED IN LABELLED COMMON
C DATA 45,IPLOT,TRUANT,TDENOM,DTIME,K,CNTX,IK,NBODY,.2,.4+.1,0,2,0,
C 295*.0,110*,.0,C,1,0,-.0035,.25,3,2/
C
C+READ CHARACTERISTICS OF PROBLEM -- RAW INPUT DATA
C
C+DEFINITION OF MAE AND NAME1
C NAMELIST /NAME/ T,SYM,ISYM,TMIN,TMAX,XMIN,XMAX,NPLOT,INUM,YDENOM,
C ZHONES,XKZ,RETA,CP,RHO,CPYR,EMISS,0Z,DTIME,NDTX,IK,ABODY,CP2,
C 3HCP4,0Z,CPZ,DTX,DTX,0Z,IK,NBODY,IX,4X2Z,RHO2,CP2,EMISS,INUM,TDENOM,
C SYST,MAE,TMIN,TMAX,YMIN,YMAX,4PLOT,WD35,WD5,A,118,IPLOT
C
C+DIMENSION TIMEF(1250),F(1250),
C READ 100,N
C 100 FORMAT(1I5)
C 101 READ 200,(TIMEF(I),F(I)),I=1,1250
C 200 FORMAT(1P10.5)
C 201 PRINT 202
C 202 PRINT (T,TIMEF(I),25X,F1,1)
C 203 PRINT 204
C 204 PRINT (T,TIMEF(I),F(I),1)
C 205 FORMAT (5X,F10.5),F10.5
C 206 J1=1
C 207 J2=1
C 208 J3=1
C 209 J4=1
C 210 READ (5,NAME1)
C
C+CALCULATE DIMENSIONLESS LUMPED PARAMETERS. MX(I) AND CI(I)
C CALL LUMP I1,MBODY,0Z
C
C+WRITE PROFILE PARAMETERS
C 211 WRITE(KH,1)
C 212 FORMAT(20HEAT TRANSFER PROGRAM MFT-24 //27M PROGRAMMED BY A.M.C.LAWSON
C 213 //26M CCAKE-NICOLSON ALGORITHM
C 214 //25M THE INPUT PARAMETERS ARE)
C 215 WRITE(KH,2)
C 216
C 217 PAGE 0002
C 218 PAGE 0003
C 219 PAGE 0004
C 220 PAGE 0005
C 221 PAGE 0006
C 222 PAGE 0007
C 223 PAGE 0008
C 224 PAGE 0009
C 225 PAGE 0010
C 226 PAGE 0011

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SECTION IN EIGHT

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200

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PAGE 0005

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PAGE 0002
 11/35/51
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 0044 00 TO 1.5
 0045 1.1 1.1 = 1F .02
 0046 C(1) = .0
 0047 H(1) = .0
 0048 R(1) = RADII(BODY + 1)
 C=CALCULATE THE DIMENSIONLESS RADIUS RII
 0049 D=1.1
 0050 1.0 RII(1) = RII(1) / (RADII(MODY+1) - RADII(1))
 0051 RETURN;
 END;

From:

To: 11/15/51

DATE: 75094

LNUO

PAGE: C003

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*STATISTICS:

FORTNIGHTLY LEVEL 21 LINEAR DATE = 75094 11/35/51
 PAGE 0001
 0001 Subroutine LINARAY(VER)
 0002 GIVES THE X(T1,T2)
 0003 S1:
 C 1 INPUT: a1, b1, c1, d1, GET TO 100
 C USE FOLLOWING IF AS Y INCREASES & INCREASES
 100 IF (X1>1.2) GOTO 200
 C USE FOLLOWING IF AS Y INCREASES & INCREASES
 C 100 IF (X1>2.3)
 200 IF (Y1>1) GOTO 300
 300 IF (Y1>1) GOTO 400
 400 RETURN
 0005 RETURN
 0007 RETURN
 0008 RETURN
 0009 RETURN
 0010 RETURN

FORTRAN IV G LEVEL 21

LINE#

PAGE 0002

11/35/51

DATE = 75094

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FORMATS IN 6 LEVEL 21

SOLVE

PAGE 0002

11/35/51

DATE = 75094

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OPTIONS IN EFFECT: NAME = SOLVE * LINECNT = 55
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 24,25,I,APLNT,11-E,LIP1,50IN,SYST,SGUT,EMBL,TIM2,LTIM)
 0002 PRINTION,TST(1150),X(110),AUS(30),NPLOT(11),Y(50),TT(150) 02200
 0003 CUMON, XBLR2/T(150),C1(150),CAT(150),MX(150),MX(150),180D(10,2)
 0004 COMMON /ALR2/ JAD(11),KZ(11),KZ(150),BET(10),CP(10),
 2P(110),EFTSS,HEQZ,COZ,XRD2,30YR(11),RIL(150),DR(10),
 2A(9),I,6(11)
 0005 CUMON, XBLR2/Y(500),10,TAU(500),Q(500),SYM,XMIN,XMAX,YMIN,YMAX,
 2I(150),T(150),T(150),T(150),T(150) 02240
 0006 COMMON /FLRA/ KOUNT,J1,J2,J3,J4,NSUP
 0007 REAL DATA(50),DATA(50) 02241
 02250
 C=CALCULATE DIMENSIONAL TIME-MEAT FLOWS PER UNIT DEPTH. TSTARS, M-S
 C=AND AVERAGE TEMPERATURE. PRINT THESE QUANTITIES.
 02260
 CALL TAVER(T11,TIP1)
 02270 TSEC = 02*2 * RMO2* CP2 * 3600./ MM2
 TIME = TAU* TSEC
 QIN = MX(11)*XK2*06.*2832*(T11) - T(21)
 QOUT = MX(11)*XK2*06.*2832*(T11) - T(11)
 MOUT=MX(11)*XK2*06.*2832*(T11) - T(11)
 MCXK2*MM2/RIC(11);
 02280
 MAMONI=MFCON
 MINMMK2=1;*XK2*RAD(11);
 0014 DO 1 I1,LIP1
 0015 1 TSTAR(I1) = (T11 - TUM)/TOENQ
 0016 0017
 0018 1 X(11) = DR(J1)*2/(DT14*E102*2);
 0019 0020 3 WRITE(4,5) TAUT
 0021 0022 5 FORMAT(1F//22H DIMENSIONLESS TIME *F7.3,10X28HMEAT FLOW PER FT,
 ZHTU/MM2FT1 *10X48COMBINED CONVECTION COEFFICIENT (BTU/HR-FT*2-F1),
 WRITE(6,7) TIME,QIN,QOUT,NGUT,MRA
 0023 7 FORMAT(22H REAL TIME (SECONDS)=E11.3+3X4HQIN=E12.3,7H QOUT=E12
 02360 0024 2,3,3K7W HR*MC*E12.3,3X3KHR*E12.3;
 0025 0026 20 FORMAT(7X,SUMQIN=*,F10.5,10X,SUMQSTR=*,F10.5,10X,SUMQOUT=*,
 2F10.5,10X,ENERGY BALANCE=*,F10.5)
 0027 9 FORMAT(30H W VALUES FOR REGIONS 1 THRU NBODY ARE,10F6.2)
 0028 0029 WRITE(6,6) MIN
 0030 8 FORMAT(25MD MIN. LATU/MR*FT*2-F1)=,10F8.2)
 0031 0032 14 C=PRINT THERMAL CONDUCTIVITIES
 14 FORMAT(14X) LIP2,XK2(11),XK2(11),X11
 14 FORMAT(14X) 2L0*/*SF10.2*5x,5F10,21)
 02444
 C=PRINT THE DIMENSIONAL TEMPERATURES
 0033 0034 11 WRITE(6,11) T(1),T(1),T(1),T(1),T(1),T(1),T(1),T(1),T(1),T(1),T(1),T(1),
 11 FORMAT(13M TIME DIMENSIONAL TEMPERATURES ARE ,6H T(1),*,F10.2/
 213* T(2) THRU T(13)*M) FOLLOW/(SF10.2*5x,SF10,21)
 02450
 0035 0036 13 WRITE(6,13) T(11),T(11),T(11),T(11),T(11),
 13 FORMAT(3M T(13,2M)=,F12.2,6*7M(LAVE),*,F12.2,
 C C=IF ANS(30)=NE..0, PRINT THE DIMENSIONLESS TEMPERATURES
 02530

FORTRAN IV G LEVEL 21
 RESULT DATE = 75094 PAGE 0002
 11/35/51

```

0037      WRITE(6,15) TSTAR(1),T1,I,(TSTAR(I),I=2,11)
0038      WRITE(I,13) I,I,TSTAR(I),TSTAR(I,IPI)
0039      FORMAT(75HCTE DIMENSIONLESS TEMPERATURES ARE/6M T(1)=,F10.2/
213- T(2) THRU T(13)QH) FOLLOW/(SF10.3*5*SF10.3)J)
0040      C PLOT OF AVG TEMP. VS TIME
0041      REAL DATAK(150), DATAV(150),
0042      ITIM = ITIM + 1
0043      TAVE = T(I,IPI)
0044      ITIM1 = ITIM
0045      ITIM2 = ITIM1
0046      ITIM3 = TAUTE*SEC
0047      IF(IPLDT(11) .EQ. 0) GO TO 18
0048      IF(TANS(150) .NE. 0) GO TO 18
0049      DO 17 J = 1, ITIM
0050      DATAV(J) = TIM(J)
0051      17 J=J+1
0052      IF(IISUP.EQ.0) GO TO 162
0053      IF(IGRANT.LT.(INSUP+1)) GO TO 18
0054      162 CALL GRAPH(CTIM, DATAK, DATAV, 3, 1, 6.0, 6.0, 0.0, 0.0,
20.0, 0.0, 6.0, 6.0, 0.0, 0.0)
0055      ITIM1=ITIM
0056      IF(IISUP.EQ.0) GO TO 18
0057      DO 161 IT=INSUP
0058      DO 160 IT=ITIM
0059      DATAK=DATAK(ITIM)
0060      DATAV=DATAV(ITIM)
0061      150 ITIM=ITIM+1
0062      161 CALL GRAPH(CTIM, DATAK, DATAV, 3, 1, 0.0, 0.0, 0.0,
20.0, 0.0, 6.0, 6.0, 0.0, 0.0)
2*TRANSIENT TEMP., TIME SECONDS, TEMPERATURE (AVE) F11.
2*TRANSIENT TEMP., VARIOUS RADII
2*CONTINUE
162 PILOT 90DE TEMP. VS TIME
163 IF(IPLDT(10) .EQ. 0) GO TO 19
164 IF(TANS(150) .NE. 0) GO TO 19
165 REAL DATAK(150), DATAV(150)
166 DO 21 J = 1, ITIM
167 DATAK(J2) = TTB(J)
168 DATAV(J2) = TIM(J)
169 21 J2=J2+1
170 IF(IISUP.EQ.0) GO TO 172
171 IF(IGRANT.LT.(INSUP+1)) GO TO 19
172 CALL GRAPH(CTIM, DATAK, DATAV, 3, 1, 6.0, 6.0, 0.0, 0.0, 0.0,
20.0, 6.0, 6.0, 6.0, 0.0, 0.0)
2*TRANSIENT AVE TEMP., CALCULATED DATA
2*ITIM=ITIM+1
173 IF(IISUP.EQ.0) GO TO 19
174 DO 171 IT=INSUP
175 DO 173 IT=ITIM
176 DATAK=DATAK(ITIM)
177 DATAV=DATAV(ITIM)
178 179

```


PR - PIAN TO G LEVEL 21

OPTIONS IN EFFECT: *010*ERICIC*SOURCE*WOLIST*NODECK*LOAD*MAP

OPTIONS IN EFFECT: NAME = RESULT * LINECOUNT * 55
STATISTICS: SOURCE STATEMENTS = 121 PROGRAM SIZE = 13794

STATISTICS: NO OF INSTRUCTIONS GENERATED:

PAGE 0004

11/30/94

RESULT

DATE = 75094

PRINTOUT IN 6 LEVEL ZI
 DATE = 75094 PAGE 0001
 11/35/51
 TAVE
 001 SUBROUTINE TAVE(I1,I1P1)
 002 COMMON /PLP1/, T1(50), C1(50), CX(150), MX(150), MXD(10,2),
 003 CALCULATE AVERAGED TEMPERATURE AND STORE IT IN T(I1P1)
 004 SUM = 0
 005 SUM2 = 0
 006 DO 39 I=1,II
 007 SUM = SUM + C(I)*T(I)
 008 SUM2 = SUM2 + C(I)*C(I)
 009 T(I1P1) = SUM/SUM2
 010 RETURN
 END

FORUM FOR GOALS

DATE 2-25-94

00000

116/117

```

OPTIONS IN EFFECT:  LOGO=FOCUS SOURCE=DECODED COLOR=MONO
OPTIONS IN EFFECT:  VALUE = 1 TIME = 1 LINECHAR = 55
SOURCE STATEMENTS = 1000000GRAM SIZE = 6000000
STATISTICS = NO OTHERS SELECTED

```


FORTRAN IV & LEVEL 21
 CHA446
 DATE = 75096
 11/35/51
 PAGE 0002

```

0032      J1 = *1(J1)
0033      DTEMP = ABS((J1)-T(J1))
0034      IF(DTEMP .GT. 0) DTEMP = 1
0035      N = N2(J1)
0036      GO TO 112+13+14+15+16+17+18
0037      112   IF(T14C .LT. 0) GO TO 11
0038      N2(J1) = -N2(J1)+15+17+20+22
0039      GO TO 11
0040      13   N2(J1) = N2(J1) + 1
0041      GO TO 11
0042      14   TA = T(J1) - 400.
0043      15   T0 = T(J1+1) + 400.
0044      N2(J1) = N2(J1) + 1
0045      16   N2(J1) = DTEMP + EXP(0
2     . N2(J1) + DTEMP + EXP(0
15     GO TO 11
0046      17   IF(4.E0 .GT. W1(J1)) = M2(J1) + K(5)
0047      18   IF(4.E0 .LT. W1(J1)) = M2(J1)
0048      19   IF(4.E0 .EQ. 0) N = -1
0049      N = N + 1
0050      GO TO 11
0051      16   GO TO 11
0052      17   GO TO 11
0053      N1  CONF1NE
0054      N11 = NNM + 1
0055      18   IF(NMODNM1 .LT. 1.E-01 .OR. (J1,E0,0) RETURN
0056      19   GO TO 11
0057      20   J1 = H1(J1)
0058      21   T(J1+1) = N2(J1) + N2(J1) + N1(J1)
0059      RETURN
0060      END
  
```

FORTRAN IV 6 LEVEL 21

CHANGE

PAGE 0003

DATE = 11/30/51

OPTIONS IN EFFECT NOID*ERCOIC*SOURCE*MOLIST*NODECK*LOAD*NCMAP
OPTIONS IN EFFECT NAME = CHANGE * LINECNT = 55
STATISTICS SOURCE STATEMENTS = 60*PROGRAM SIZE = 1952
STATISTICS NO DIAGNOSTICS GENERATED

FORTRAN IV O LEVEL 21

BLV DATA DATE = 75094

PAGE 0002

OPTIONS IN EFFECT NOOPT=FOCODE SOURCE=MOLIST NOCODECK LOAD=ROMAP
OPTIONS IN EFFECT NAME = BLV DATA LINECNT = 55
STATISTICS NO DIAGNOSTICS GENERATED

STATISTICS NO DIAGNOSTICS THIS STEP

FORA-LEVEL LINKAGE EDITOR OPTIONS SPECIFIED LIST,LET,NOXREF,SCRF
DEFAULT OPTION(S) USED - SIZE=19280,8192)

DOES NOT EXIST. PUT HAS BEEN ADDED TO DATA SET

422-51001	0
450-00000	0
450-01001	1-00000
452-00000	1-00000
452-51001	0
540-00000	0
540-01001	1-00000
542-50000	0
542-51001	0
570-00000	0
570-01001	1-00000
572-50000	0
572-51001	0
605-00000	0
606-01001	1-00000
692-50000	0
692-51001	0
693-00000	0
693-01001	1-00000
694-50000	0
694-51001	0
695-00000	0
695-01001	1-00000
696-50000	0
696-51001	0
697-50000	0
697-51001	0
720-00000	0
720-01001	1-00000
722-50000	0
722-51001	0
750-00000	0
750-01001	1-00000
752-50000	0
752-51001	0
760-00000	0
760-01001	1-00000
782-50000	0
782-51001	0
810-00000	0
810-01001	1-00000
842-50000	0
842-51001	0
870-00000	0
870-01001	1-00000
912-50000	0
912-51001	0
940-00000	0
940-01001	1-00000
972-50000	0
972-51001	0
990-00000	0
990-01001	1-00000
992-50000	0
992-51001	0
994-00000	0
994-01001	1-00000
996-00000	0
996-01001	1-00000
998-50000	0
998-51001	0

932-51001	0.0
960-00000	0.0
960-01001	1.00000
962-50000	1.00000
962-51001	0.0
990-00000	0.0
990-01001	1.00000
992-50000	1.00000
992-51001	0.0
1080-00000	0.0
1080-01001	1.00000
1082-50000	1.00000
1082-51001	0.0
1110-00000	0.0
1110-01001	1.00000
1112-50000	1.00000
1112-51001	0.0
1140-00000	0.0
1140-01001	1.00000
1142-50000	1.00000
1142-51001	0.0
1170-00000	0.0
1170-01001	1.00000
1172-50000	1.00000
1172-51001	0.0
1200-00000	0.0
1200-01001	1.00000
1202-50000	1.00000
1202-51001	0.0
1230-00000	0.0
1230-01001	1.00000
1232-50000	1.00000
1232-51001	0.0
1260-00000	0.0
1260-01001	1.00000
1262-50000	1.00000
1262-51001	0.0
1290-00000	0.0
1290-01001	1.00000
1292-50000	1.00000
1292-51001	0.0
1320-00000	0.0
1320-01001	1.00000
1322-50000	1.00000
1322-51001	0.0
1350-00000	0.0
1350-01001	1.00000
1352-50000	1.00000
1352-51001	0.0
1380-00000	0.0
1380-01001	1.00000
1382-50000	1.00000
1382-51001	0.0
1410-00000	0.0
1410-01001	1.00000
1412-50000	1.00000
1412-51001	0.0
1440-00000	0.0
1440-01001	1.00000
1442-50000	1.00000

1442-51001	0.0
1470-00000	0.0
1470-01201	1.00000
1472-50000	1.00000
1472-51001	0.0
1500-00000	0.0
1500-01001	1.00000
1502-50000	1.00000
1502-51001	0.0
1530-00000	0.0
1530-01201	1.00000
1532-50000	1.00000
1532-51001	0.0
1700-00000	0.0

HEAT TRANSFER PROGRAM HT-2A
PROGRAMMED BY A. M. CLAUING
CHANK-NICOLSON ALGORITHM
SESSION = 1 JUNE 1970

THE PENTITENTIALS

DIMENSIONLESS TIME = 0.052 MEAT FLOW PER FT (BTU/HR-FT²)
REAL TIME (SECONDS) = 0.100E+00 QIN= 0.30E+05 QOUT= 0.10E+01 HR= 0.54E+00

SUMTIME= 15.05021 SUMQSTIME= 54.86342 SUBROUT= 0.00000 ENERGY BALANCE= -26.53564

W VALUES FOR REGIONS 1 THRU NINEY ARE 16.21

MIN BTU/HR-FT²-F1= 561.40
THE Dermal CONDUCTIVITIES FOR KXZ(121 THRU KXZ(151 FOLLOW
26.47 25.75 26.47 26.94 27.23
27.40 27.40 27.60

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00 T(2) THRU T(16) FOLLOW
416.40 294.50 211.27 157.03 123.13
80.44 80.18 60.07 80.03 80.02
T(17)= 80.00 T(AVE)= 174.28

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00 T(2) THRU T(16) FOLLOW
418.70 296.504 211.270 157.030 123.131
80.455 80.180 60.070 80.029 80.020
T(17)= 80.00 T(AVE)= 106.28

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0010
THE CURRENT DIMENSIONLESS TIME IS = 0.2505

DIMENSIONLESS TIME = 0.259 MEAT FLOW PER FT (BTU/HR-FT²)
REAL TIME (SECONDS) = 0.50E+01 QIN= 0.422E+05 QOUT= 0.170E+02 HR= 0.58E+00

SUMTIME= 65.2234 SUMQSTIME= 97.91985 SUBROUT= 0.00594 ENERGY BALANCE= -50.14029

W VALUES FOR REGIONS 1 THRU NINETY ARE 6.36

MIN BTU/HR-FT²-F1= 571.80
THE Dermal CONDUCTIVITIES FOR KXZ(121 THRU KXZ(151 FOLLOW
23.10 24.04 24.04 25.38 25.84
27.19 27.27 27.32 27.36
T(17)= 60.00 T(AVE)= 105.13

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00 T(2) THRU T(16) FOLLOW
507.76 481.76 403.29 336.65 293.37
127.76 118.56 112.18 108.85 107.71
T(17)= 60.00 T(AVE)= 105.13

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00 T(2) THRU T(16) FOLLOW
507.763 481.777 403.291 336.646 293.374
127.761 118.542 112.177 108.845 107.707

T(1)= 171.00 MEAN= 175.13

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS TIME IS = 0.0020
THE CURRENT DIMENSIONLESS TIME IS = 0.0035

DIMENSIONLESS TIME = 2.520 MEAT FLOW PER FT (BTU/HR-FT) =
REAL TIME (SECO.051= 0.103E+02 VINE 0.397E+05 QOUT= 0.746E+02
CONFINED CONVECTION COEFFICIENT (BTU/HR-FT*E2=F):
MR+KC= 0.173E+01 HR= 0.725E+00

SUMS1= 121.539362

SUMS2= 148.456602 SUMOUT= 0.66755 ENERGY BALANCE= -22.20175

* VALUES FOR REGIONS 1 THRU NINETY ARE 4.18

MIN (BTU/HR-FT*E2=F)= 561.00
THERMAL CONDUCTIVITIES FOR TX(12) THRU TX(21) FOLLOW
22.49 23.26 23.07 24.52 24.97 25.15 25.66 25.92 26.13
26.62 26.52 26.59 26.63 26.63 26.63 26.63 26.63 26.29

6 THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW
678.98 577.681 493.666 435.967 382.96 339.89 294.20 270.75 256.67 231.33
216.22 204.95 197.16 192.66 191.17
T(17)= 80.00 TRAVEL= 275.77

6 THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW
678.981 577.681 493.666 435.967 382.959 339.886 294.201 274.748 256.674 231.334
216.226 204.947 197.159 192.659 191.169
T(17)= 80.00 TRAVEL= 275.77

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0000
THE CURRENT DIMENSIONLESS TIME IS = 1.0005

DIMENSIONLESS TIME = 1.040 MEAT FLOW PER FT (BTU/HR-FT) =
REAL TIME (SECO.051= 0.201E+02 QIN= 0.337E+05 QOUT= 0.232E+03
CONFINED CONVECTION COEFFICIENT (BTU/HR-FT*E2=F):
MR+KC= 0.212E+01 HR= 0.122E+01

SUMS1= 222.10665 SUMS2= 239.08818 SUMOUT= 0.48493 ENERGY BALANCE= -7.86691

* VALUES FOR REGIONS 1 THRU NINETY ARE 2.00
MIN (BTU/HR-FT*E2=F)= 561.60
THERMAL CONDUCTIVITIES FOR TX(12) THRU TX(21) FOLLOW
21.62 22.19 22.79 23.27 23.67 24.40 24.28 24.51 24.70 24.85
26.97 25.06 25.12 25.16

THE DIMENSIONAL TEMPERATURES ARE
T(1)= 1563.00
T(2) THRU T(16) FOLLOW

T(1)= 1561.00
 T(2) THRU T(16) FOLLOW
 T(17)= 60.00

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1561.00
 T(2) THRU T(16) FOLLOW
 T(17)= 60.00

TIME	TEMPERATURE
1	634.54
2	366.30
3	362.71
4	361.26
5	437.11
6	437.01
7	437.01
8	437.01
9	437.01
10	437.01
11	437.01
12	437.01
13	437.01
14	437.01
15	437.01
16	437.01
17	60.00

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1561.00
 T(2) THRU T(16) FOLLOW
 T(17)= 60.00

TIME	TEMPERATURE
1	634.54
2	366.30
3	362.71
4	361.26
5	437.11
6	437.01
7	437.01
8	437.01
9	437.01
10	437.01
11	437.01
12	437.01
13	437.01
14	437.01
15	437.01
16	437.01
17	60.00

DIMENSIONLESS TIME = 1.562
 REAL TIME (SECONDS) = 0.301E+02

SUMDOUT= 310.9115

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 22.00

T(1)= 23.48

T(2)= 21.78

T(3)= 22.20

T(4)= 22.55

T(5)= 23.82

T(6)= 23.82

T(7)= 23.82

T(8)= 23.82

T(9)= 23.82

T(10)= 23.82

T(11)= 23.82

T(12)= 23.82

T(13)= 23.82

T(14)= 23.82

T(15)= 23.82

T(16)= 23.82

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

T(8)= 21.24

T(9)= 21.24

T(10)= 21.24

T(11)= 21.24

T(12)= 21.24

T(13)= 21.24

T(14)= 21.24

T(15)= 21.24

T(16)= 21.24

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 1.562

REAL TIME (SECONDS) = 0.301E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 22.00

T(1)= 23.48

T(2)= 21.78

T(3)= 22.20

T(4)= 22.55

T(5)= 23.82

T(6)= 23.82

T(7)= 23.82

T(8)= 23.82

T(9)= 23.82

T(10)= 23.82

T(11)= 23.82

T(12)= 23.82

T(13)= 23.82

T(14)= 23.82

T(15)= 23.82

T(16)= 23.82

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

T(8)= 21.24

T(9)= 21.24

T(10)= 21.24

T(11)= 21.24

T(12)= 21.24

T(13)= 21.24

T(14)= 21.24

T(15)= 21.24

T(16)= 21.24

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 1.562

REAL TIME (SECONDS) = 0.301E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 22.00

T(1)= 23.48

T(2)= 21.78

T(3)= 22.20

T(4)= 22.55

T(5)= 23.82

T(6)= 23.82

T(7)= 23.82

T(8)= 23.82

T(9)= 23.82

T(10)= 23.82

T(11)= 23.82

T(12)= 23.82

T(13)= 23.82

T(14)= 23.82

T(15)= 23.82

T(16)= 23.82

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

T(8)= 21.24

T(9)= 21.24

T(10)= 21.24

T(11)= 21.24

T(12)= 21.24

T(13)= 21.24

T(14)= 21.24

T(15)= 21.24

T(16)= 21.24

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

T(8)= 21.24

T(9)= 21.24

T(10)= 21.24

T(11)= 21.24

T(12)= 21.24

T(13)= 21.24

T(14)= 21.24

T(15)= 21.24

T(16)= 21.24

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

T(8)= 21.24

T(9)= 21.24

T(10)= 21.24

T(11)= 21.24

T(12)= 21.24

T(13)= 21.24

T(14)= 21.24

T(15)= 21.24

T(16)= 21.24

T(17)= 60.00

TIME INCREMENT DOUBLED. NEW DIMENSIONLESS INCREMENT IS = 0.0080

TIME CURRENT DIMENSIONLESS TIME IS = 2.0000

DIMENSIONLESS TIME = 2.000

REAL TIME (SECONDS) = 0.601E+02

N VALUES FOR REGIONS 1 THRU 16000 ARE

MIN (BTU/HR-FEET-SQFT)= 541.80

TOTAL CONDUCTIVITIES FOR EQUATIONS 151 THROUGH 155 = 21.00

T(1)= 20.41

T(2)= 21.24

T(3)= 21.24

T(4)= 21.24

T(5)= 21.24

T(6)= 21.24

T(7)= 21.24

22.43 22.66 22.91 22.74

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00
T(2)= THRU T(16) FOLLOW
— 971.02 904.12 431.10 808.27 773.03
— 454.17 650.03 444.14 640.01 639.51
T(17)= 80.00 T(18)= 598.60

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00
T(2)= THRU T(16) FOLLOW
971.393 904.125 431.100 808.271 773.026
358.166 650.079 444.343 640.906 639.507
T(17)= 80.00 T(18)= 598.600

DIMENSIONLESS TIME = 2.6200 MEAT FLOW PER FT (BTU/HR-FT)
REAL TIME (SECONDS)= 0.501E+07 Q1IN= 0.94E+03 COMBINED CONVECTION COEFFICIENT (BTU/HR-FT+02-F)
Q2IN= 0.22E+05 QOUT= 0.94E+03 HR= 0.263E+01

SUMQIN= 454.35742 SUMQSTRA= 645.24678 SUMQOUT= 5.19321 ENERGY BALANCE= 0.86177

E VALUES FOR REGIONS 1 THRU NINE ARE 1.04
MIN (BTU/HR-FT) = 501.00
THEAL CONDUCTIVITIES FOR SK212 THRU SK215:
19.22 19.74 20.15 20.48 20.75 FOLLOW
21.63 21.69 21.74 21.77 20.97 21.16 21.31 21.44 21.55

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00
T(2)= THRU T(16) FOLLOW
988.71 984.76 938.21 900.59 869.66
760.16 760.91 755.76 752.51 751.03
T(17)= 80.00 T(18)= 503.93

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00 MEAT FLOW PER FT (BTU/HR-FT)
T(2)= THRU T(16) FOLLOW Q1IN= 0.200E+05 QOUT= 0.12E+04 COMBINED CONVECTION COEFFICIENT (BTU/HR-FT+02-F)
— 1044.271 940.764 938.208 900.583 869.663 HR= 0.31E+01
748.162 760.922 755.755 752.515 751.060 SUMQIN= 513.60229 ENERGY BALANCE= 1.78636
T(17)= 80.00 T(18)= 503.93 E VALUES FOR REGIONS 1 THRU NINE ARE 1.04
MIN (BTU/HR-FT)= 501.00

THEORETICAL CONDUCTIVITIES FOR X=2 (2) FOLLOW X=2 (15) FOLLOW
 16.46 16.14 16.49 19.74
 20.00 20.00 20.00 20.00

THE ONE-DIMENSIONAL TEMPERATURES ARE

T(1)= 1561.00
 T(2), THRU T(16), FOLLOW
 1165.31 1054.34 1013.40 966.23 952.92
 950.71 950.67 951.72 949.07 947.15
 T(17)= 80.00 FOLLOW
 T(18)= 89.56

THE ONE-DIMENSIONLESS TEMPERATURES ARE

T(1)= 1561.00
 T(2), THRU T(16), FOLLOW
 1165.710 1054.379 1013.402 960.206 952.456
 949.031 956.468 951.320 948.652 947.154
 T(17)= 80.00 FOLLOW
 T(18)= 89.56

DIMENSIONLESS FLUX = 3.632 HEAT FLOW PER FT (BTU/HRS-FT)

REAL TIME (SECONDS) = 0.700E+07 Q1W = 2.177E+05 Q2W = 0.154E+04

S/NO/ONE 545.0318

HEAT FLOW = 579.35571

W VALUES FOR HEATLOSS 1 THRU 16 ARE 1.04

WITH (BTU/HRS-FT) = 545.0318

THEORETICAL CONDUCTIVITIES FOR X=2 (2) FOLLOW X=2 (15) FOLLOW

16.22 16.02 16.04 16.14 19.40
 20.10 20.15 20.19 20.22

THE ONE-DIMENSIONAL TEMPERATURES ARE

T(1)= 1561.00
 T(2), THRU T(16), FOLLOW
 1159.73 1112.45 1077.40 1047.06 1023.46
 963.40 937.00 912.04 893.06 873.45
 T(17)= 60.00 FOLLOW

THE ONE-DIMENSIONLESS TEMPERATURES ARE

T(1)= 1561.00
 T(2), THRU T(16), FOLLOW
 1159.725 1113.345 1077.108 1047.063 1023.450
 963.368 937.369 912.394 893.035 873.454
 T(17)= 60.00 FOLLOW

TIME FOR INPUT DOUBLED. NEW ONE-DIMENSIONLESS ELEMENT IS = 0.0160

THE CURRENT ONE-DIMENSIONLESS TIME IS = 0.0160

HEAT FLOW = 579.35571

COMBINED CONVECTION COEFFICIENT (BTU/HRS-FT^{0.25}-F)

MR=HC = 0.466E+01 WR = 0.366E+01

OPENING TIMES TIME = 0.161

HEAT FLOW = 579.35571

COMBINED CONVECTION COEFFICIENT (BTU/HRS-FT^{0.25}-F)

REAL TIME (SECONDS)= 0.302E+02 QIN= 0.156E+05 QOUT= 0.184E+04 HR+HC= 0.514E+01 HR= 0.414E+01
 SUMQIN= 611.88949 SUMQSTR= 577.513E-07 SUMQOUT= 16.82306 ENERGY BALANCE= 2.86689
 MIN (BTU/MR-FT**2-F)= 561.90
 MAX (BTU/MR-FT**2-F)= 561.90
 M VALUES FOR REGIONS 1 THRU 4 BODY ARE 0.52
 REGIONAL CONDUCTIVITIES FOR XZ(2) THRU XZ(15) FOLLOW
 17.41 18.17 18.45 18.68 18.87 FOLLOW
 19.49 19.54 19.58 19.60 19.61
 19.49 19.54

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1206.63 1165.72 1133.66 1107.68 1086.23
 1014.43 1008.92 1004.78 1001.91 1000.23
 T(17)= 80.00 T(AVE)= 1039.31

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1206.627 1165.719 1133.657 1107.686 1086.226
 1014.435 1008.917 1004.777 1001.911 1000.233
 T(17)= 80.00 T(AVE)= 1039.31

50
 DIMENSIONLESS TIME= 4.672 HEAT FLOW PER FT (BTU/MR-FT)
 REAL TIME (SECONDS)= 0.901E+02 QIN= 0.139E+05 QOUT= 0.212E+04 COMBINED CONNECTION COEFFICIENT (BTU/MR-FT**2-F)
 SUMQIN= 652.11725 SUMQSTR= 609.14966 SUMQOUT= 22.26405 HR+HC= 0.558E+01 HR= 0.458E+01
 M VALUES FOR REGIONS 1 THRU 4 BODY ARE 0.52
 REGIONAL CONDUCTIVITIES FOR XZ(2) THRU XZ(15) FOLLOW
 17.47 17.79 18.04 18.24 18.41 FOLLOW
 18.98 19.02 19.03 19.05 19.06
 T(17)= 80.00 T(AVE)= 1095.61

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1245.56 1239.11 1230.42 1157.33 1138.14
 1073.32 1068.19 1064.26 1061.44 1059.66
 T(17)= 80.00 T(AVE)= 1095.61

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1245.56 1209.110 1190.519 1157.331 1138.164
 1073.321 1068.187 1064.258 1061.443 1059.664
 T(17)= 80.00 T(AVE)= 1095.61

DIMENSIONLESS TIME = 5.2E-07 HEAT FLOW PER FT (BTU/HR-FT²)
REAL TIME (SECONDS) = 5.1205E-03 QINW = 0.101E-05 QOUT = 0.269E-04

SUMQIN = 519.94 J/S5 SUMQOUT = 319.94 J/S5

W VALUES FOR REGIONS & 100% WIGHT ARE 0.52

MIN. THERMAL CONDUCTIVITIES FOR 100% WIGHT ARE 5.1E-08

16.71	16.94	27.12	17.27	17.39
17.02	17.36	17.49	17.62	

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1553.00	T(2) THRU T(16) FOLLOW			
1132.97	1304.01	1285.59	1264.64	1254.52
1205.00	1206.75	1197.23	1194.47	1192.39
T(17) = 10.03	T(CLAY) = 1221.61			

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1563.00	T(2) THRU T(16) FOLLOW			
1312.64	1306.411	1295.594	1285.635	1254.520
1205.00	1205.151	1197.236	1194.667	1192.393
T(17) = 8.00	T(CLAY) = 1221.61			

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1563.00	T(2) THRU T(16) FOLLOW			
1315.51	1365.06	1346.96	1335.73	1324.65
1284.12	1280.43	1277.11	1274.72	1272.42
T(17) = 6.00	T(CLAY) = 1227.40			

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1563.00	T(2) THRU T(16) FOLLOW			
1315.51	1365.06	1346.96	1335.73	1324.65
1284.12	1280.43	1277.11	1274.72	1272.42
T(17) = 6.00	T(CLAY) = 1227.40			

DIMENSIONLESS TIME = 7.7E-07 HEAT FLOW PER FT (BTU/HR-FT²)
REAL TIME (SECONDS) = 0.150E-03 QINW = 0.775E-04 QOUT = 0.341E-04

SUMQIN = 524.51029 SUMQOUT = 722.51004

W VALUES FOR REGIONS & 100% WIGHT ARE 0.52

16.75	16.93	16.57	16.68	16.76
17.13	17.17	17.19	17.22	

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1563.00	T(2) THRU T(16) FOLLOW			
1315.51	1365.06	1346.96	1335.73	1324.65
1284.12	1280.43	1277.11	1274.72	1272.42
T(17) = 6.00	T(CLAY) = 1227.40			

THE DIMENSIONLESS TEMPERATURES ARE

T(1) = 1563.00	T(2) THRU T(16) FOLLOW			
1315.51	1365.06	1346.96	1335.73	1324.65
1284.12	1280.43	1277.11	1274.72	1272.42
T(17) = 6.00	T(CLAY) = 1227.40			

THIS INCORRECT OUTPUT IS DUE TO THE INCONSISTENCIES IN ELEMENT 15 & 0.0323

THE CURRENT DIMENSIONLESS TIME IS = 8.00002

DIMENSIONLESS TIME = 0.344
REAL TIME (SECONDS) = 0.135E+03 QIN= 0.638E+06 QOUT= 0.379E+04 COMBINED CONVECTION COEFFICIENT (BTU/HR-FT²-F)
SUNQSTR= 743.12891 HR= 0.787E+01 MR= 0.647E+01

M VALUES FOR REGIONS 1 THRU NADY ARE 0.26
MIN (BTU/HR-FT²-F)= 561.80
THERMAL CONDUCTIVITIES FOR EACH REGION FOLLOW
15.67 16.12 16.24 16.33 16.41 16.48 16.54 16.60 16.64 16.68
16.72 16.75 16.80

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW
1417.22 1480.42 1387.09 1376.13 1365.89 1355.96 1352.08 1346.06 1340.77 1336.10
1331.98 1322.33 1325.12 1322.30 1319.84
T(17)= 80.00 T(AVE)= 1342.90

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW
1432.29 1400.41 1387.00 1376.13 1365.89 1355.96 1352.08 1346.06 1340.77 1336.10
1372.97 1326.13 1325.12 1322.30 1319.84
T(17)= 80.00 T(AVE)= 1342.90

DIMENSIONLESS TIME = 10.912
REAL TIME (SECONDS) = 0.210E+03 QIN= 0.555E+04 QOUT= 0.492E+04 COMBINED CONVECTION COEFFICIENT (BTU/HR-FT²-F)
SUNQSTR= 763.50000 HR= 0.817E+01 MR= 0.717E+01

M VALUES FOR REGIONS 1 THRU NADY ARE 0.26
MIN (BTU/HR-FT²-F)= 561.80
THERMAL CONDUCTIVITIES FOR EACH REGION FOLLOW
15.61 15.93 16.04 16.12 16.19 16.25 16.31 16.35 16.40 16.43
16.67 16.50 16.52 16.55

THE DIMENSIONAL TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW
1435.28 1421.66 1410.03 1401.42 1392.27 1385.23 1379.08 1373.64 1368.80 1364.47
1362.58 1357.08 1353.93 1351.08 1348.51
T(17)= 80.00 T(AVE)= 1370.16

THE DIMENSIONLESS TEMPERATURES ARE

T(1)= 1563.00
T(2) THRU T(16) FOLLOW

1636.242 1.21.53 1410.924 1400.416 1392.269
 1360.532 1.57.02 1351.926 1.51.079 1348.512
 T(17)= 60.00 T(AVE)= 1370.36

DIMENSIONLESS TIME = 12.494
 REAL TIME :SECOND: = 3.241E+13
 SUMIN= 976.65063 SUMSTA= 772.54940
 QIN= 0.405E+00 QOUT= 0.416E+04
 MR+HC= 0.834E+01 HR= 0.734E+01
 ENERGY BALANCE= 3.77726

MIN BTU/HR-FT²-F = 561.80
 THERMAL CONDUCTIVITIES FOR XKZ(2) THRU XKZ(15)
 15.71 15.82 15.92 15.99 FOLLOW
 16.12 16.35 16.38 16.40

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1447.42 1434.16 1423.54 1414.73 1407.23
 1371.43 1364.01 1359.88 1356.02 1355.39
 T(17)= 60.00 T(AVE)= 1396.49

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1447.517 1439.177 1423.543 1414.729 1407.225
 1377.429 1370.010 1370.854 1366.019 1365.387
 T(17)= 60.00 T(AVE)= 1386.44

DIMENSIONLESS TIME = 13.504
 REAL TIME :SECOND: = 0.2560E+01
 SUMIN= 1063.74585 SUMSTA= 770.32959
 QIN= 0.449E+04 QOUT= 0.422E+04
 MR+HC= 0.842E+01 HR= 0.742E+01
 ENERGY BALANCE= 3.70582

MIN BTU/HR-FT²-F = 561.80
 THERMAL CONDUCTIVITIES FOR XKZ(2) THRU XKZ(15)
 15.67 15.78 15.87 15.94 FOLLOW
 16.26 16.29 16.31 16.34

THE DIMENSIONLESS TEMPERATURES ARE
 T(1)= 1563.00
 T(2) THRU T(16) FOLLOW
 1452.221 1439.41 1429.10 1420.71 1413.47
 1384.47 1381.08 1377.97 1375.09 1372.44
 T(17)= 60.00 T(AVE)= 1393.27

THE DIMENSIONLESS TEMPERATURES ARE

$T(1) = 1563.00$
 $T(2) = T_{\text{RHO}} T(16)$ FOLLOW
 1452.210 1439.407 1429.161 1420.710 1413.475
 1394.464 1381.061 1377.967 1375.063 1372.435
 $T(17) = 80.00$ $T(\text{AVE}) = 1393.25$

DIMENSIONLESS TIME = 15.56
 REAL TIME (SECONDS) = 0.307E+01 MEAT FLOW PER FT (BTU/MR-Ft) = 0.405E+04
 SURFACE=1056.1651 CONSIDER CONVECTION COEFFICIENT (BTU/MR-Ft**2-F)
 MIN (BTU/MR-Ft**2-F) = 561.80 QIN= 0.405E+04 QOUT= 0.405E+04 HR= 0.051E+01
 SURFACE= 760.92163 HR+HC= 0.751E+01

SUMQUT= 237.73356 ENERGY BALANCE= 3.55157

W VALUES FOR REGIONS 1 THRU NINETEEN ARE 0.26
 THE LOCAL CONDUCTIVITIES FOR XKZ(2) T-RH XKZ(15) FOLLOW
 15.42 15.72 15.41 15.05 15.99 15.04 16.08
 16.10 16.21 16.24 16.26

THE DIMENSIONAL TEMPERATURES ARE:

$T(1) = 1563.00$
 $T(2) = T_{\text{RHO}} T(16)$ FOLLOW
 1457.02 1445.77 1436.06 1427.04 1421.07
 1393.02 1389.63 1386.56 1383.69 1381.00
 $T(17) = 80.00$ $T(\text{AVE}) = 1401.41$

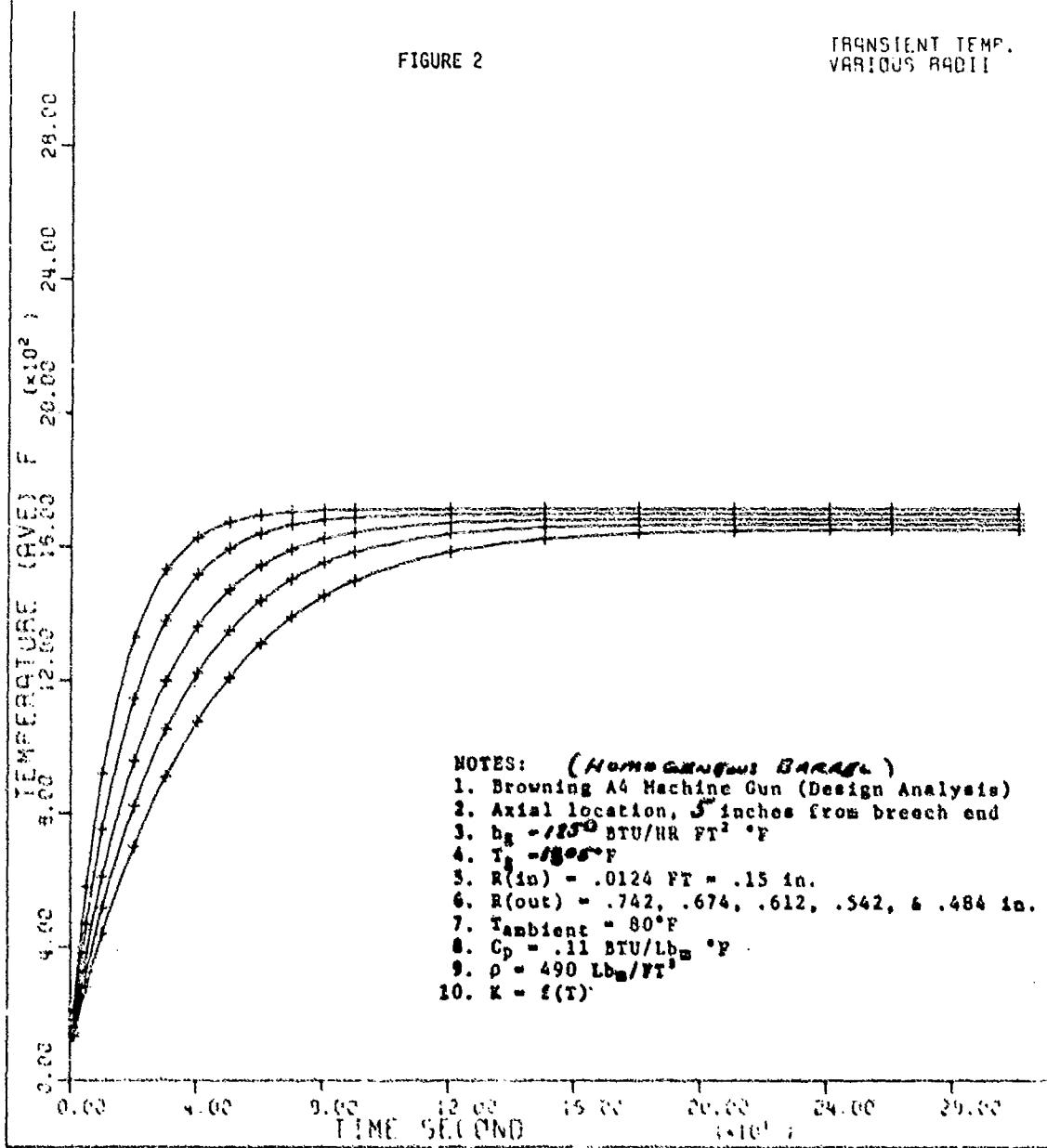
THE DIMENSIONLESS TEMPERATURES ARE:

$T(1) = 1563.00$
 $T(2) = T_{\text{RHO}} T(16)$ FOLLOW
 1457.02 1445.77 1436.06 1427.04 1421.07
 1393.02 1389.63 1386.56 1383.69 1381.00
 $T(17) = 80.00$ $T(\text{AVE}) = 1401.41$

APPENDIX 3

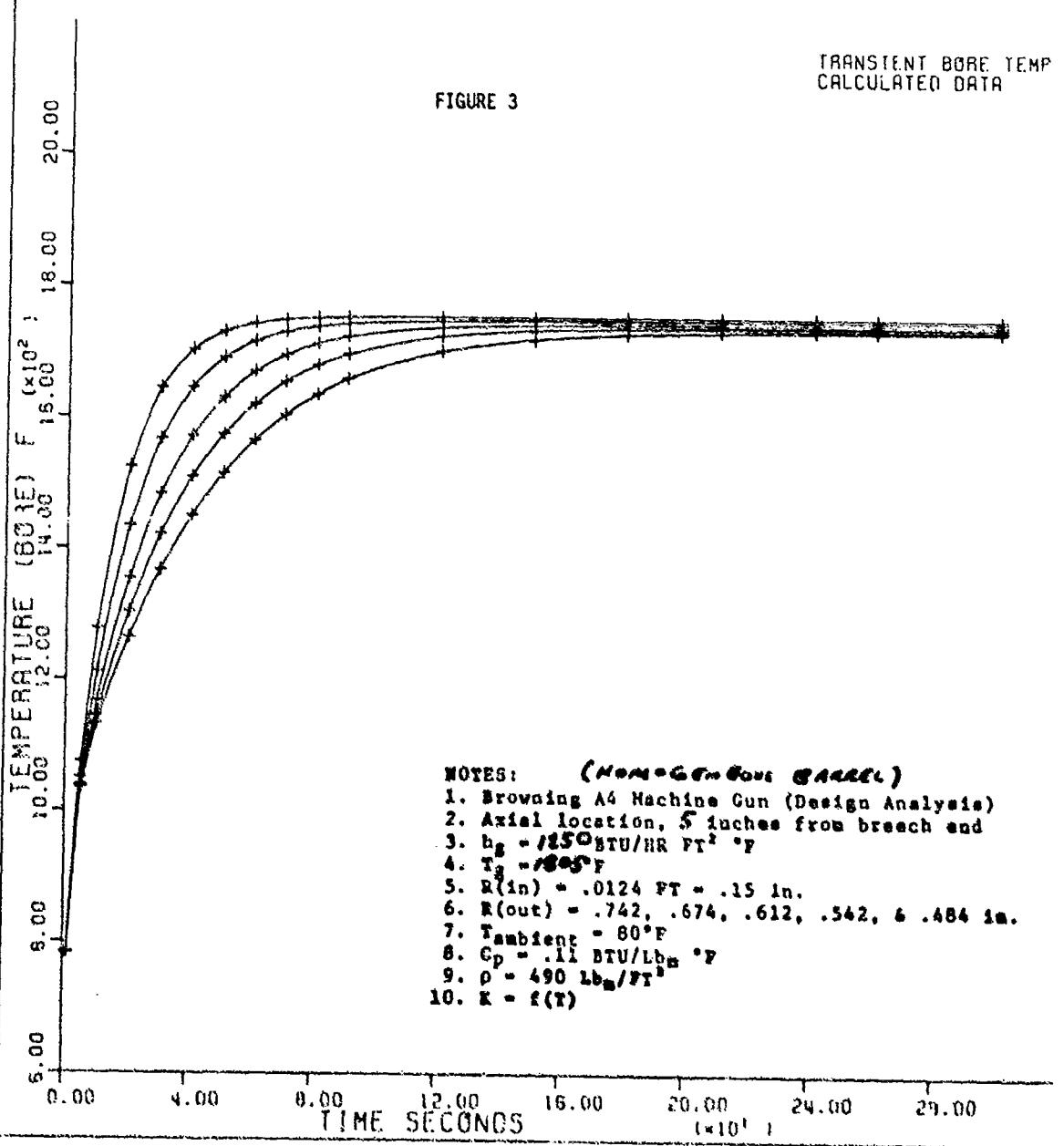
FIGURE 2

TRANSIENT TEMP.
VARIOUS RADII



TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 3



TRANSIENT
CALCULATED DATA

FIGURE 4

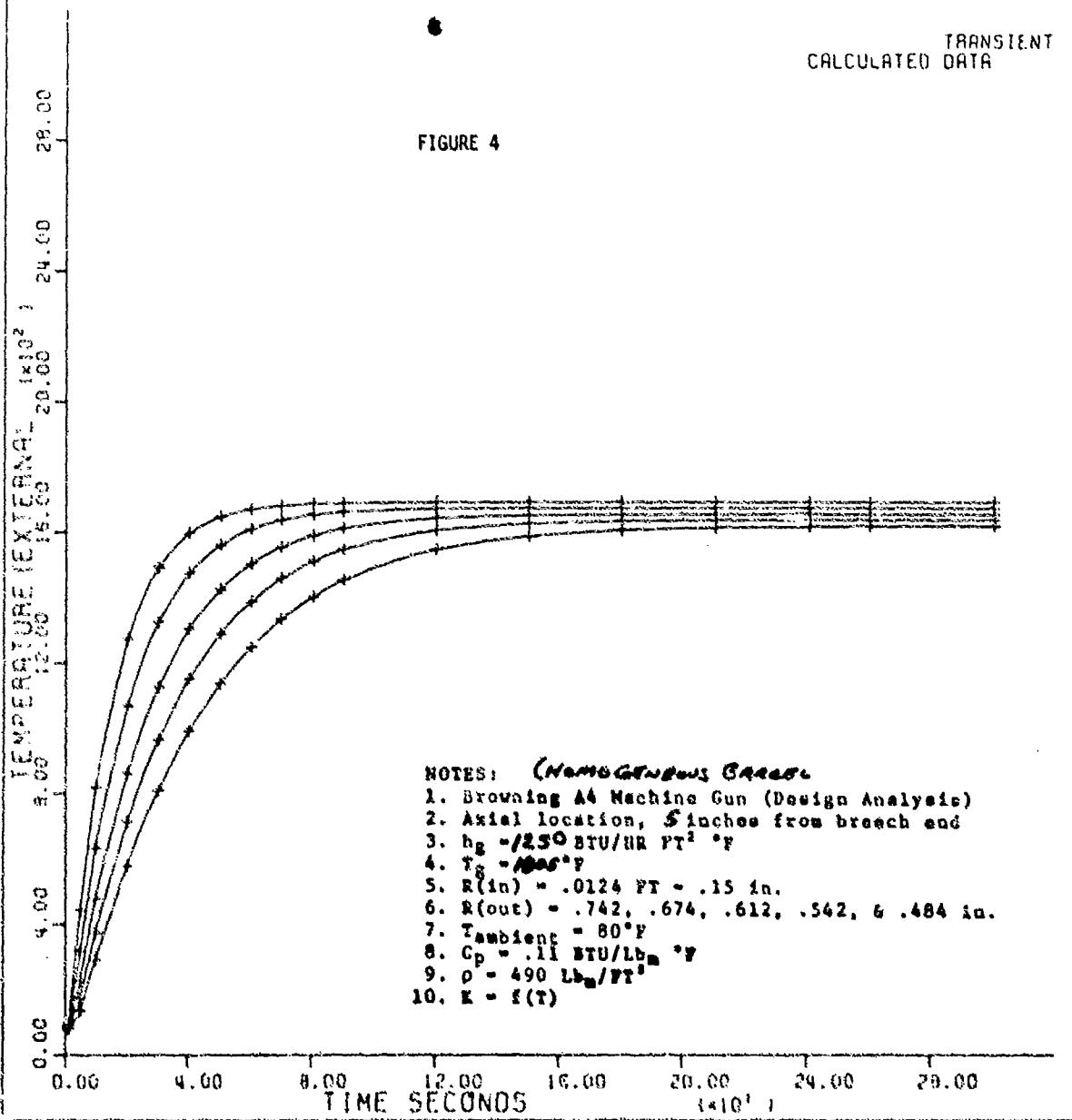
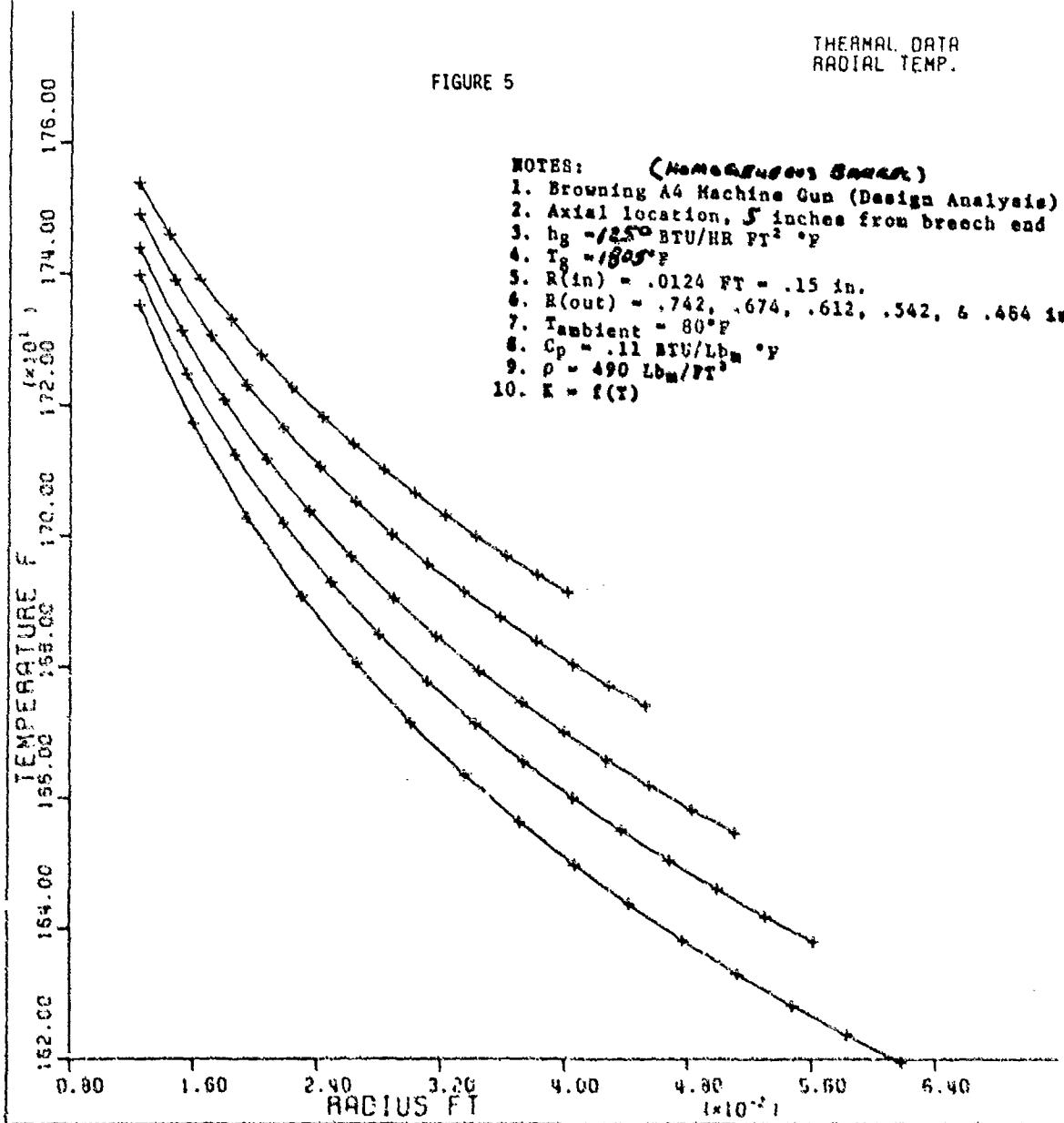


FIGURE 5

THERMAL DATA
RADIAL TEMP.

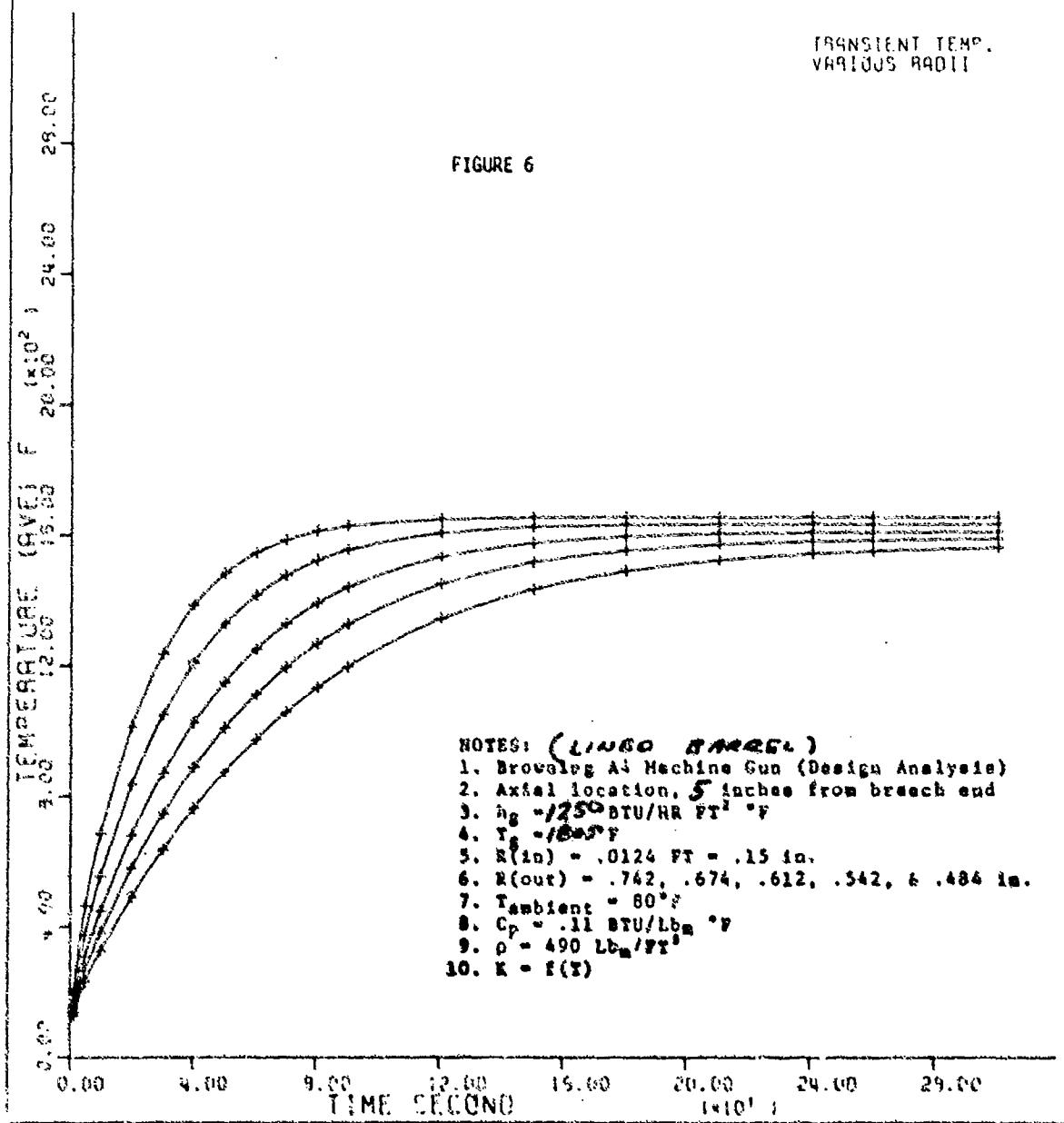
NOTES: (Numerous Errors)

1. Browning A4 Machine Gun (Design Analysis)
2. Axial location, 5 inches from breech end
3. $h_g = 1250 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$
4. $T_b = 180^\circ\text{F}$
5. $R(\text{in}) = .0124 \text{ FT} = .15 \text{ in.}$
6. $R(\text{out}) = .742, .674, .612, .542, \text{ & } .464 \text{ in.}$
7. $T_{\text{ambient}} = 80^\circ\text{F}$
8. $C_p = .11 \text{ BTU/Lb}_m \text{ }^\circ\text{F}$
9. $\rho = 490 \text{ Lb}_m/\text{FT}^3$
10. $K = f(T)$



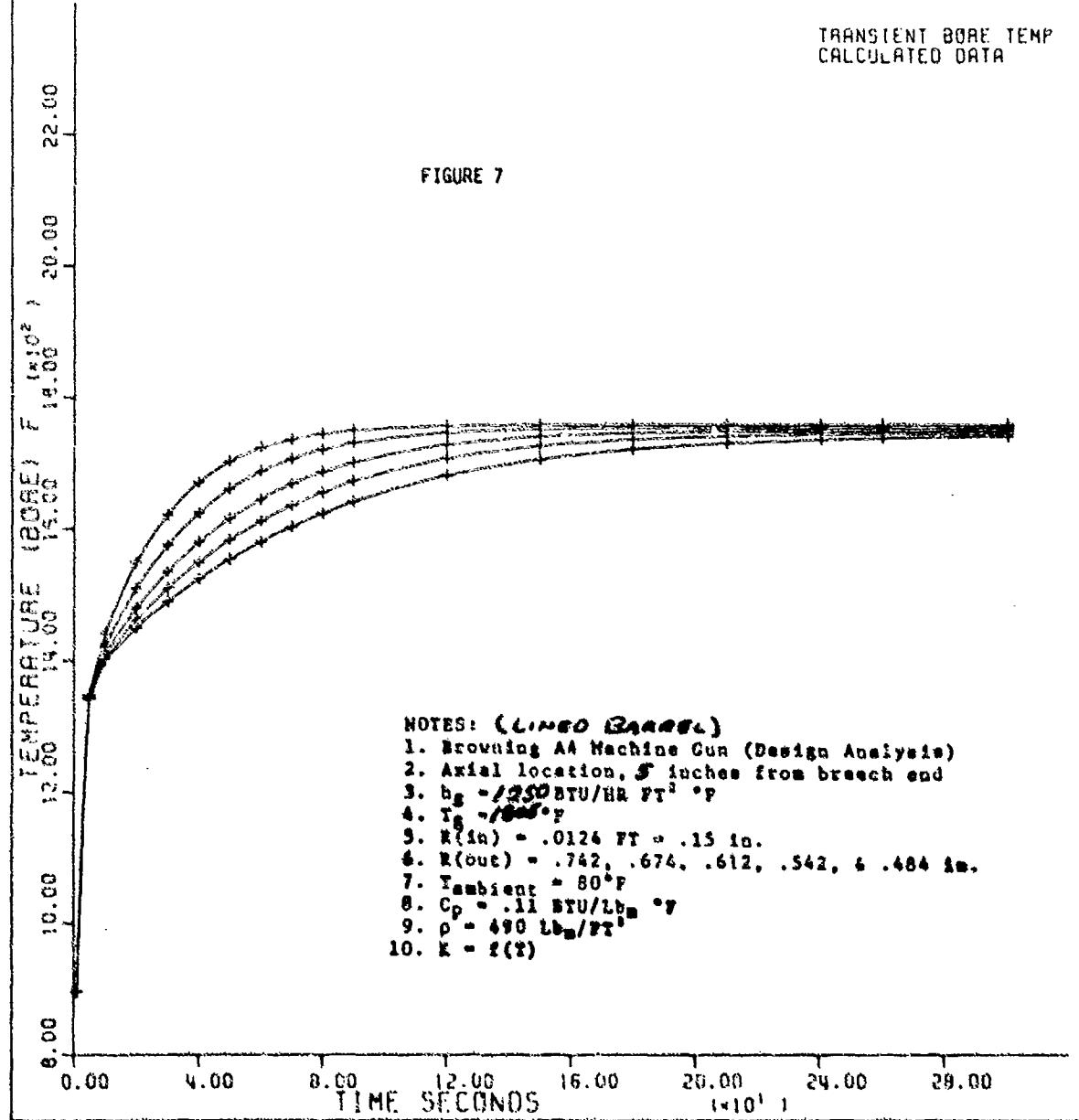
TRANSIENT TEMP.
VARIOUS RADII

FIGURE 6



TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 7



TRANSIENT
CALCULATED DATA

FIGURE 8

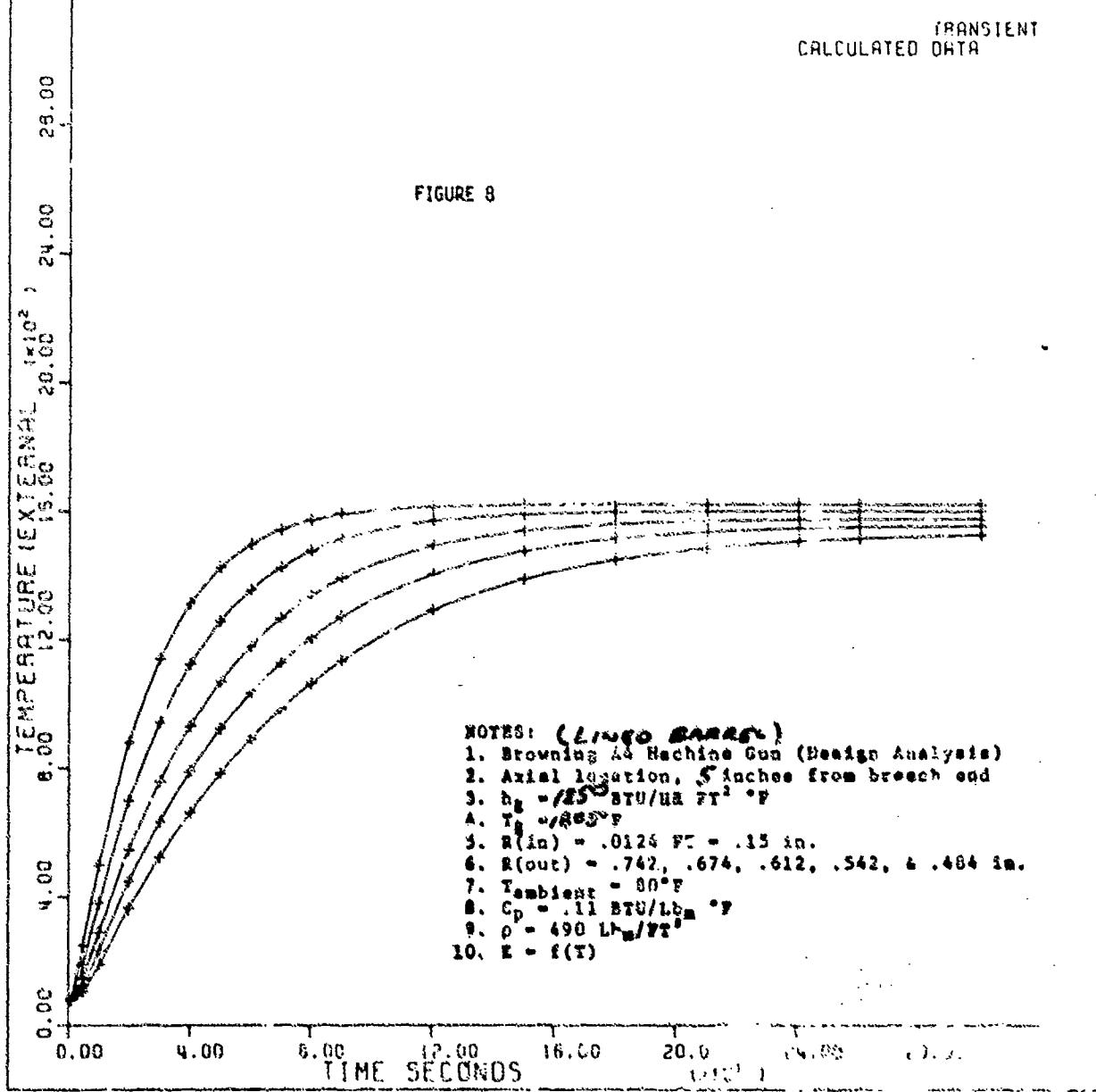
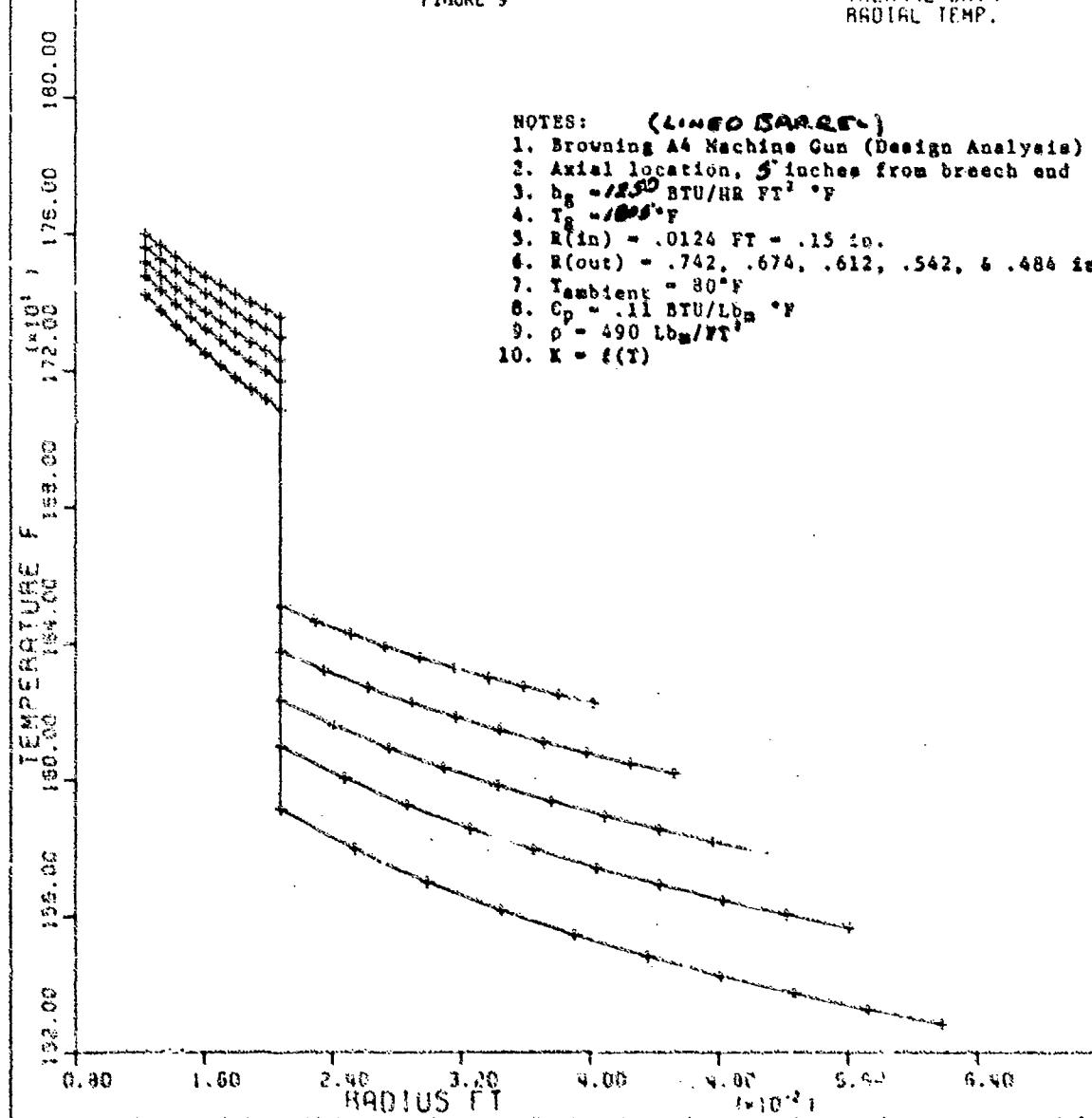


FIGURE 9

THERMAL DATA
RADIAL TEMP.

- NOTES: (LINED BARRELS)
1. Browning A4 Machine Gun (Design Analysis)
 2. Axial location, 5 inches from breech end
 3. $h_g = 1000 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$
 4. $T_g = 1000^\circ\text{F}$
 5. $R(\text{in}) = .0124 \text{ FT} = .15 \text{ in.}$
 6. $R(\text{out}) = .742, .674, .612, .542, \text{ & } .484 \text{ in.}$
 7. $T_{\text{ambient}} = 80^\circ\text{F}$
 8. $C_p = .11 \text{ BTU/LB} \text{ }^\circ\text{F}$
 9. $\rho = 490 \text{ LB}_m/\text{FT}^3$
 10. $K = f(T)$



TRANSIENT TEMP.
VARIOUS RADII

FIGURE 10

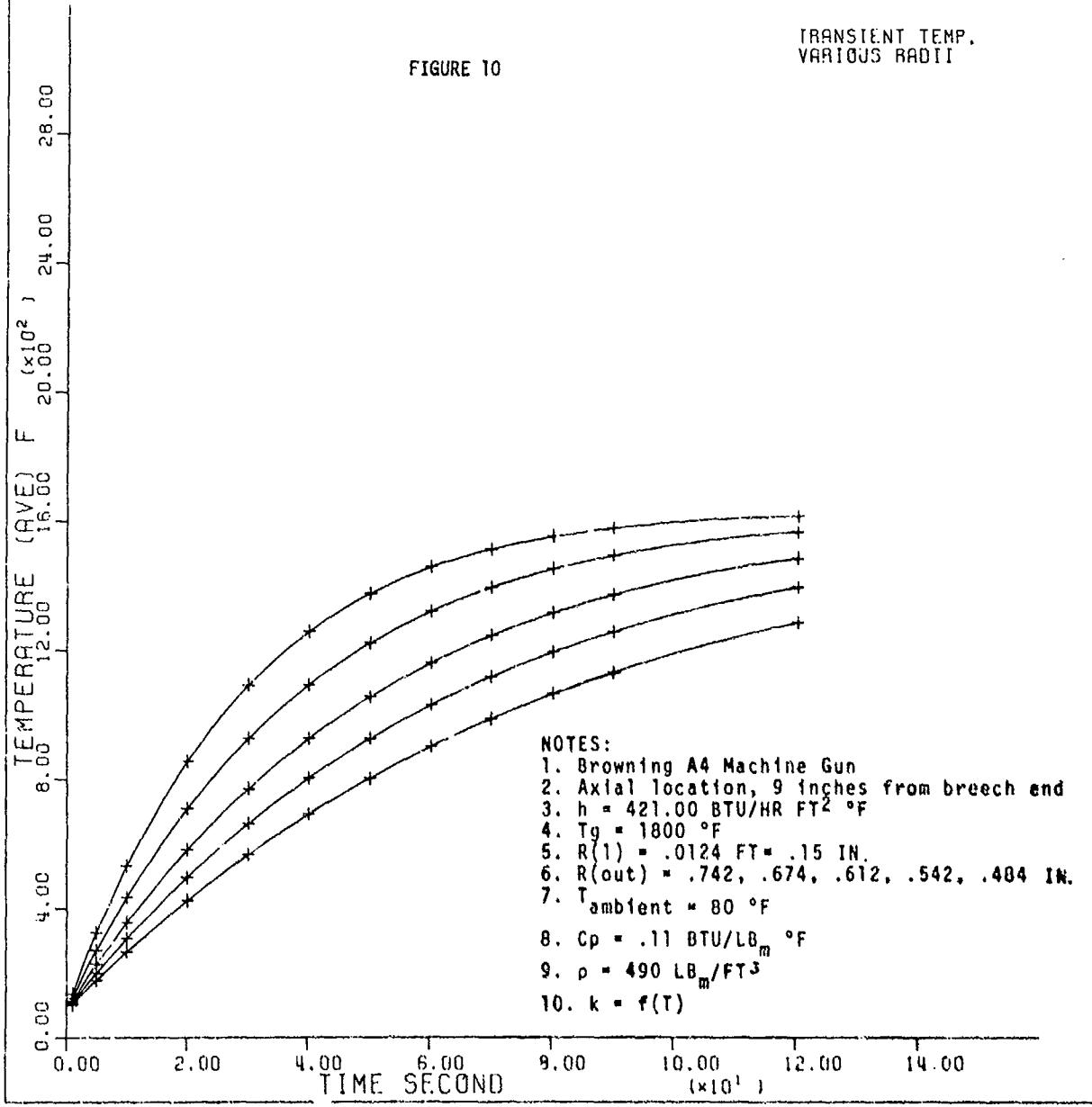


FIGURE 11

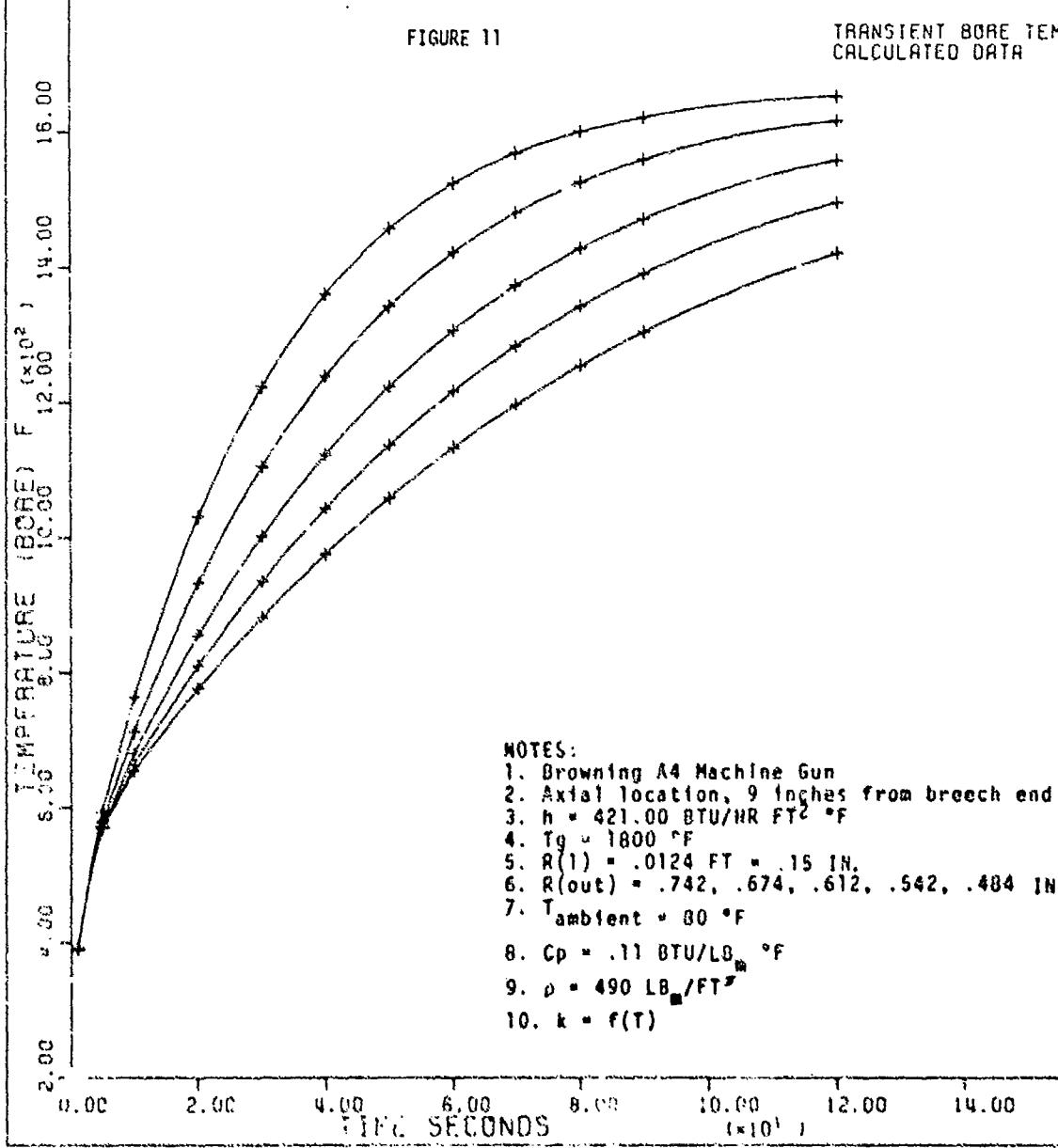
TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 12

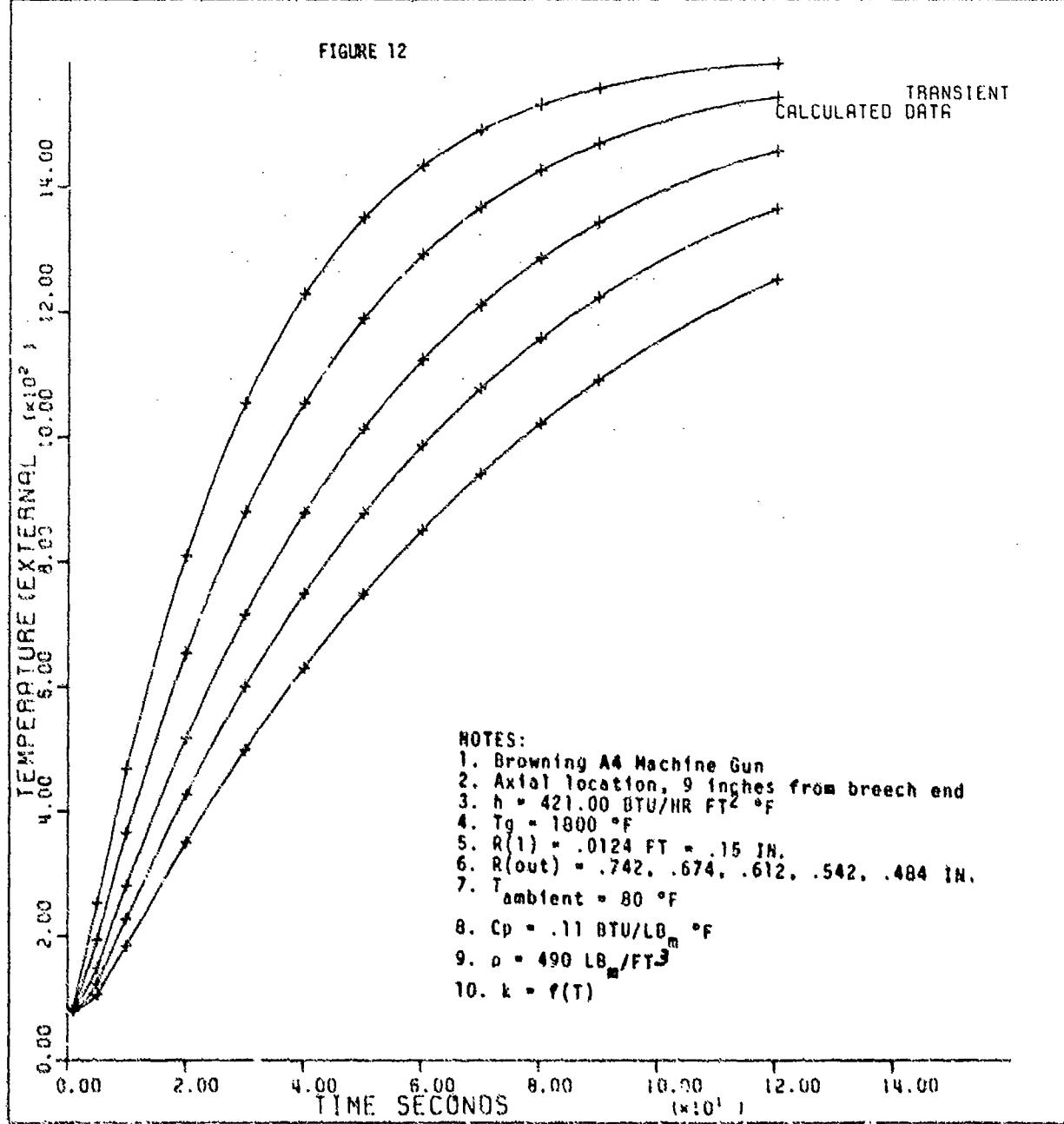
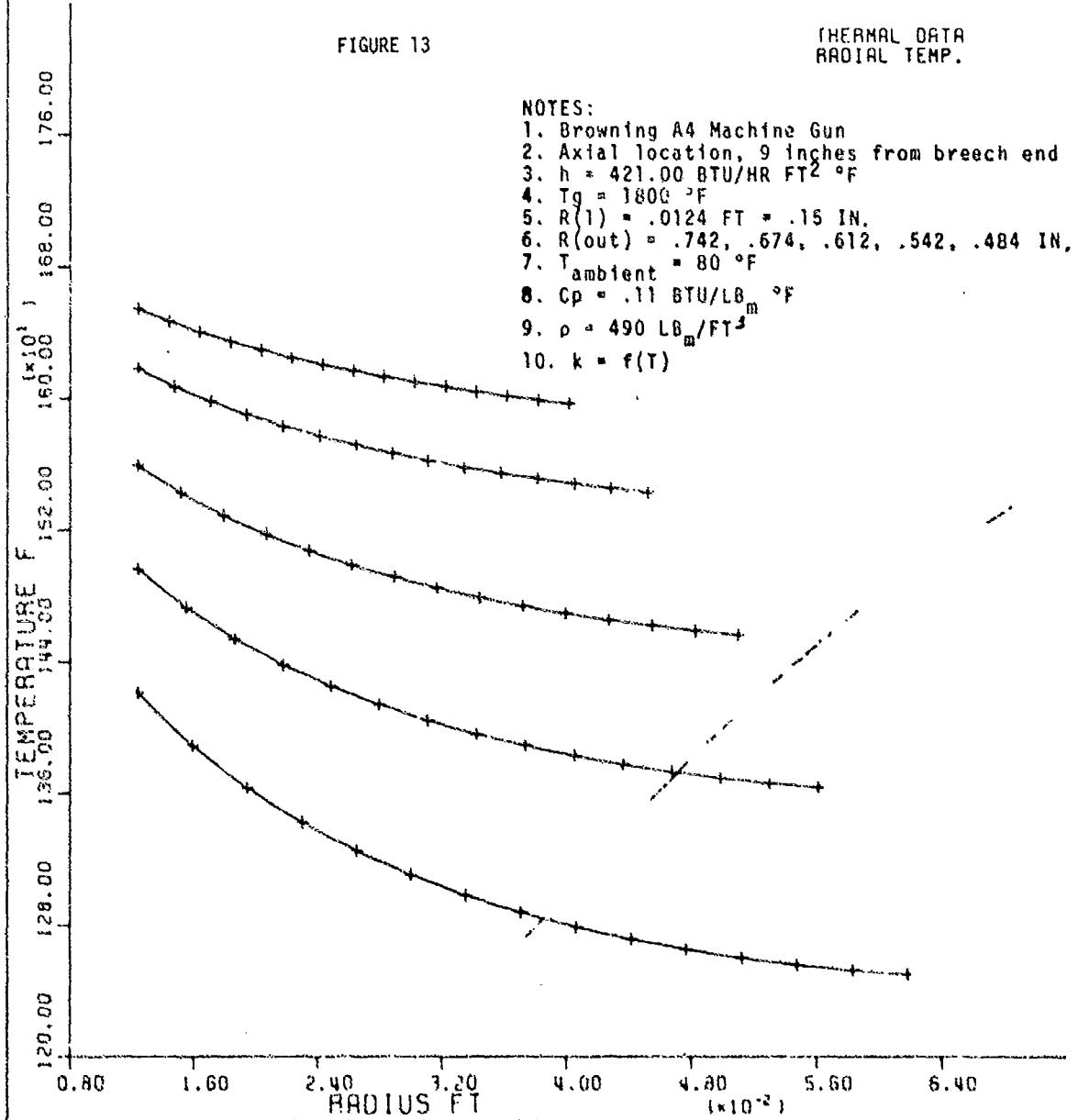


FIGURE 13

THERMAL DATA
RADIAL TEMP.

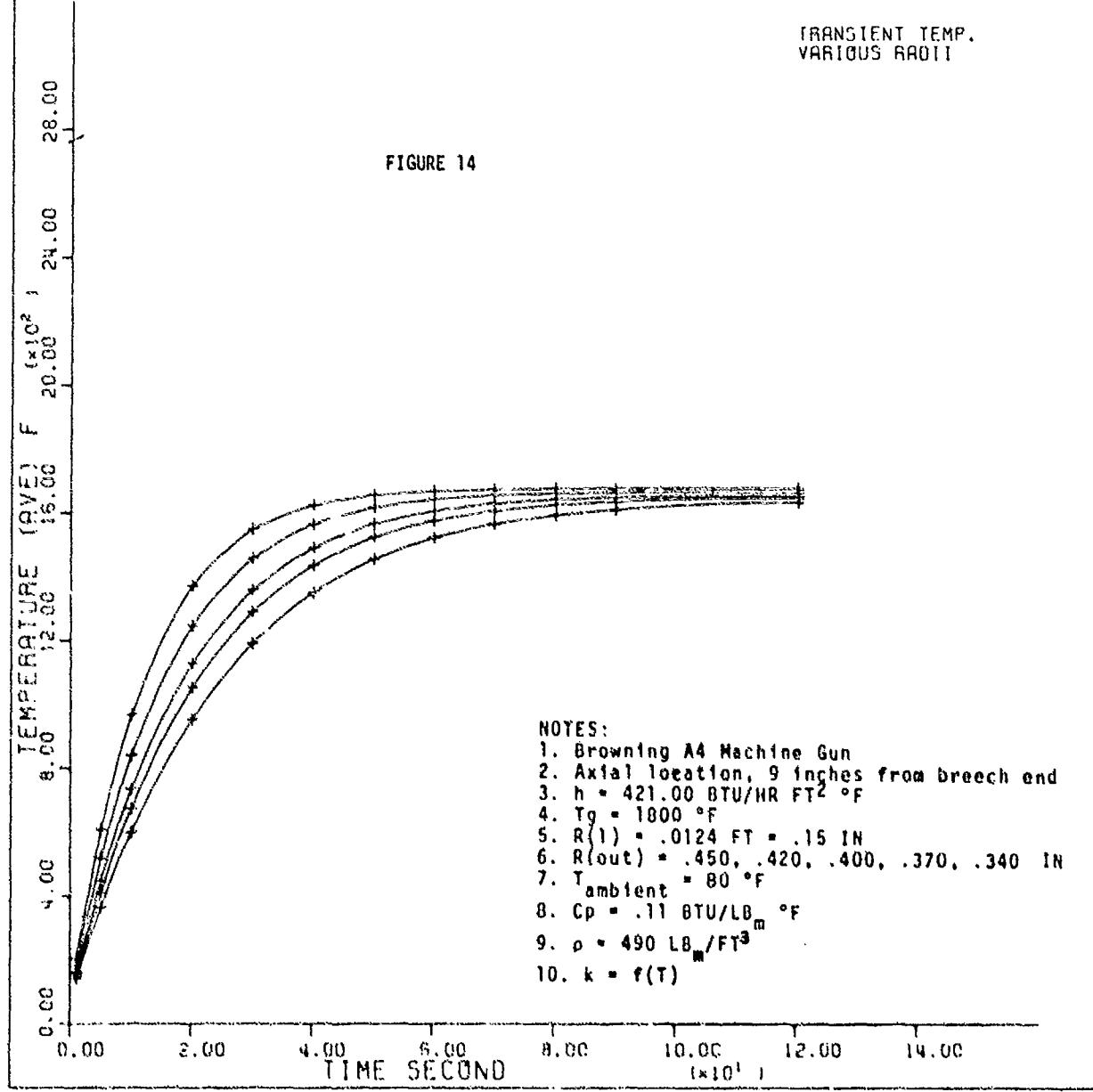
NOTES:

1. Browning A4 Machine Gun
2. Axial location, 9 inches from breech end
3. $h = 421.00 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$
4. $T_g = 1800 \text{ }^\circ\text{F}$
5. $R(1) = .0124 \text{ FT} = .15 \text{ IN.}$
6. $R(\text{out}) = .742, .674, .612, .542, .484 \text{ IN.}$
7. $T_{\text{ambient}} = 80 \text{ }^\circ\text{F}$
8. $C_p = .11 \text{ BTU/LB}_m \text{ }^\circ\text{F}$
9. $\rho = 490 \text{ LB}_m/\text{FT}^3$
10. $k = f(T)$



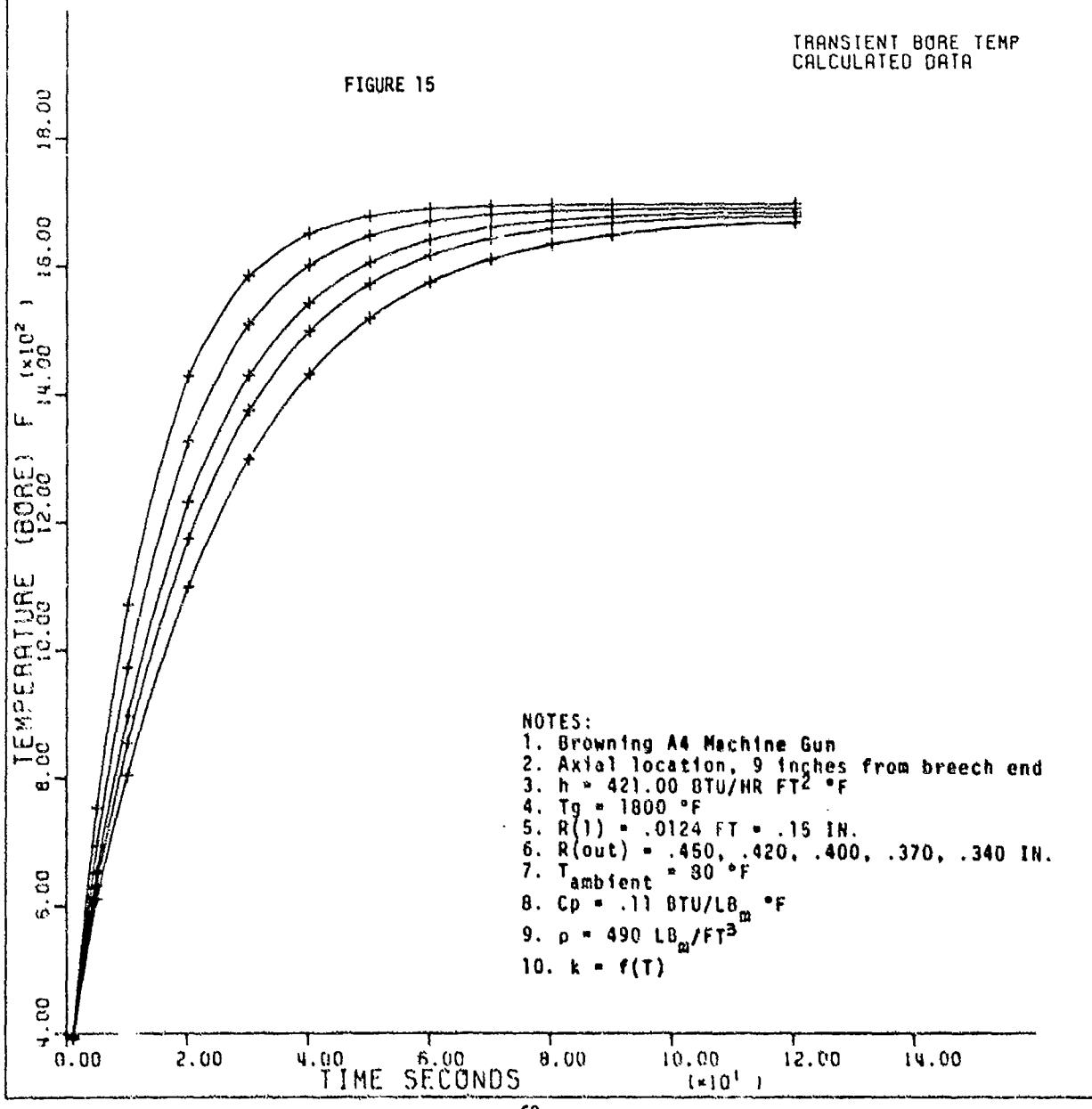
TRANSIENT TEMP.
VARIOUS RADII

FIGURE 14



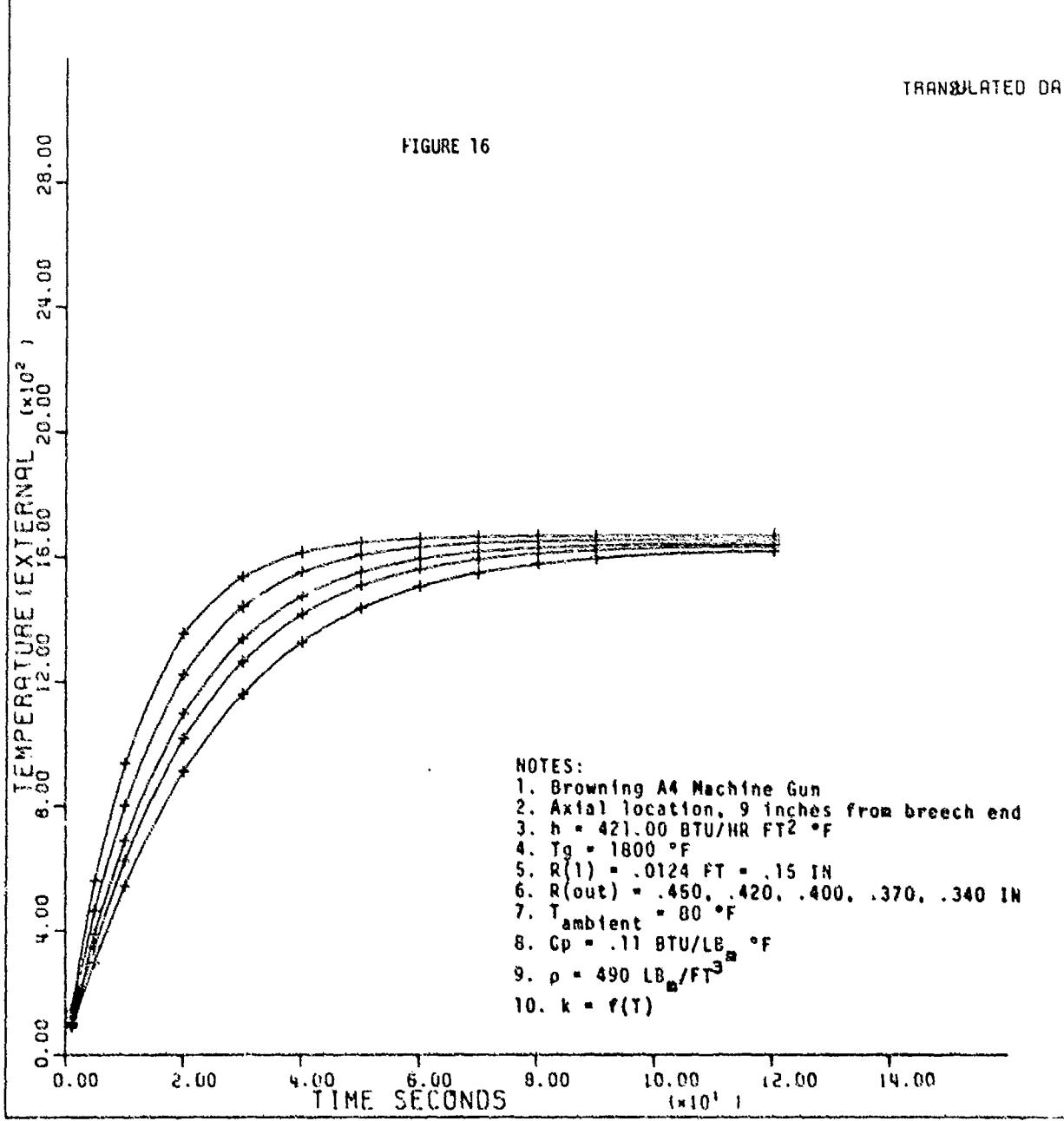
TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 15



TRANSLATED DATA

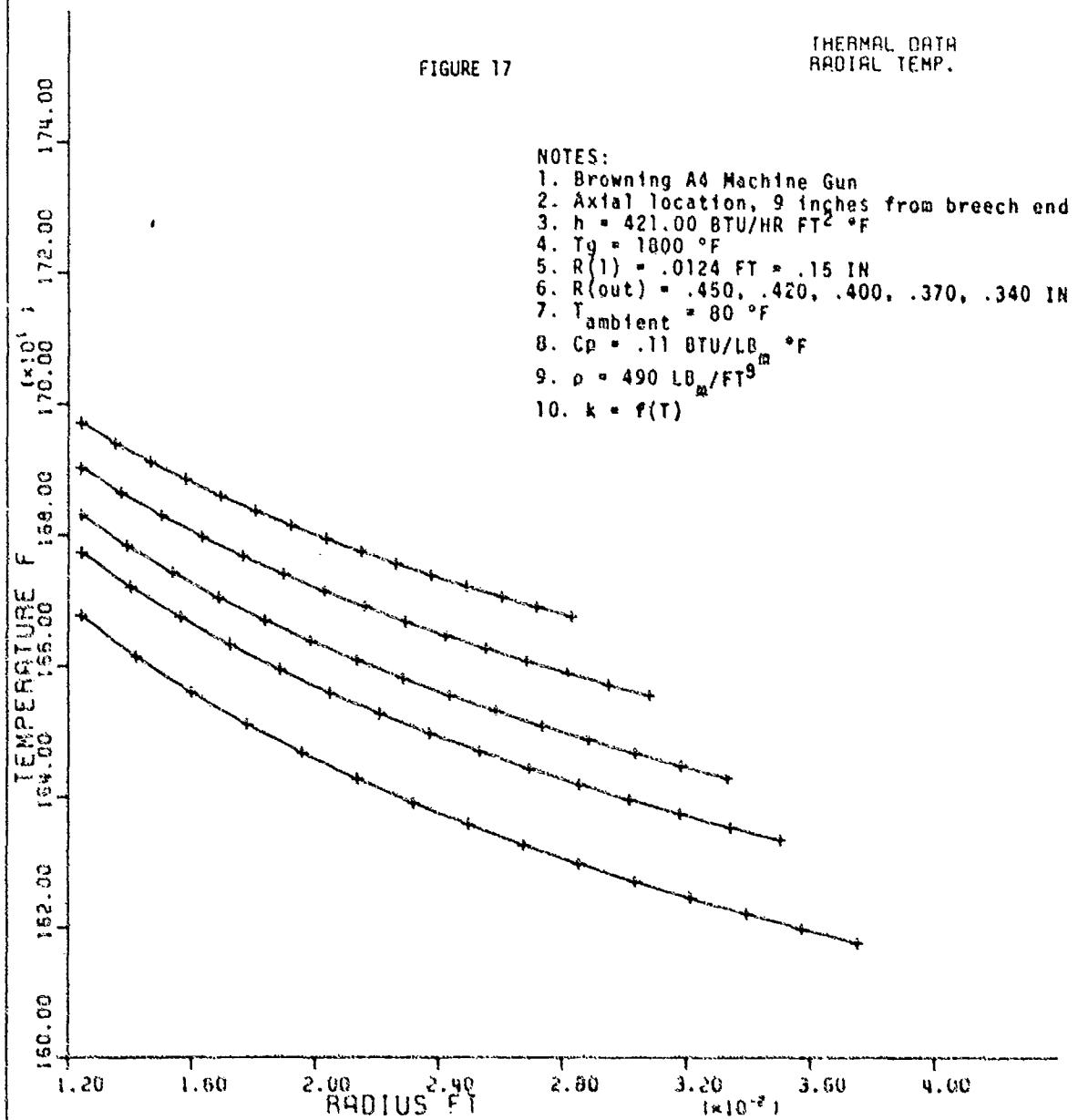
FIGURE 16

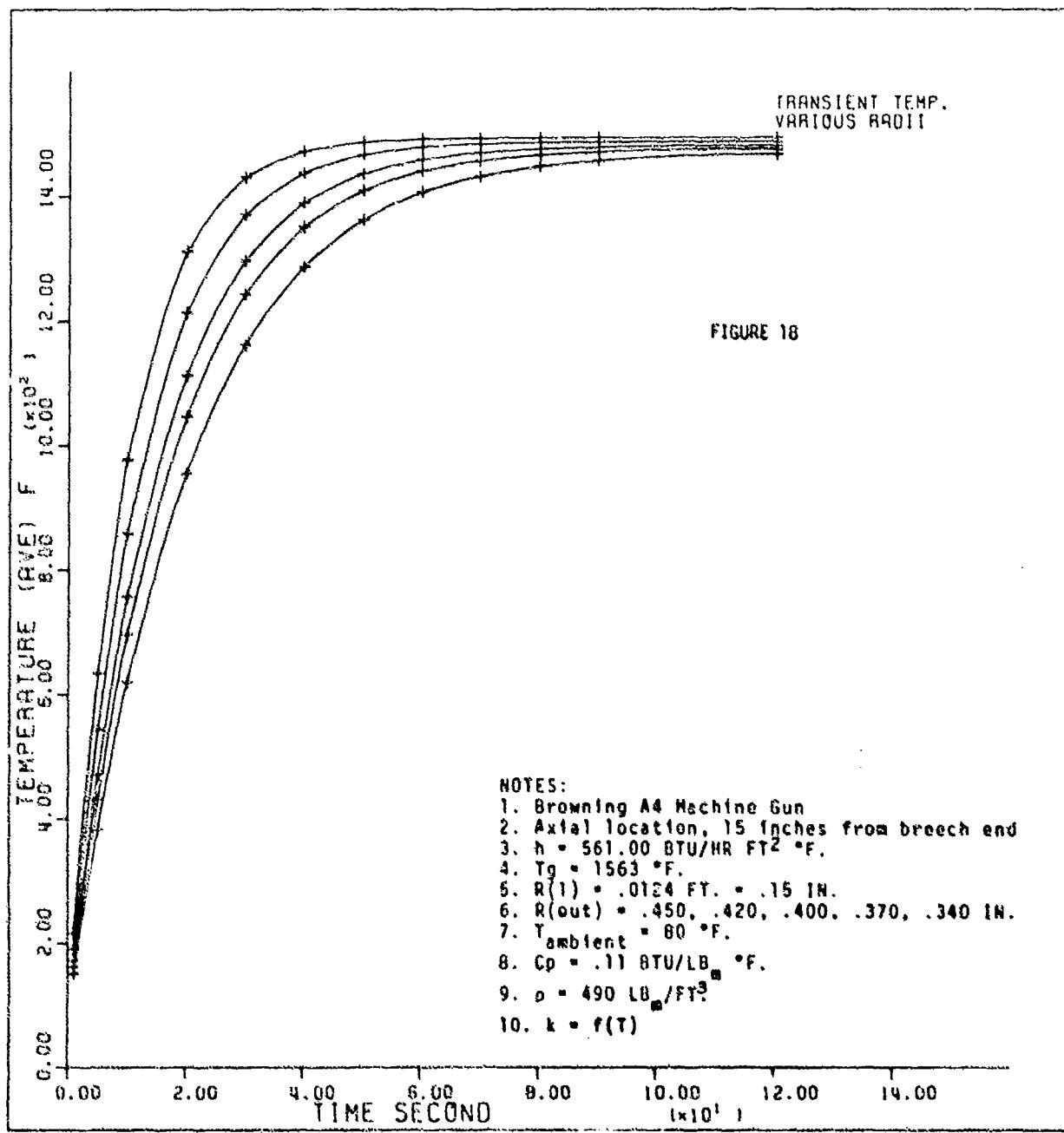


THERMAL DATA
RADIAL TEMP.

FIGURE 17

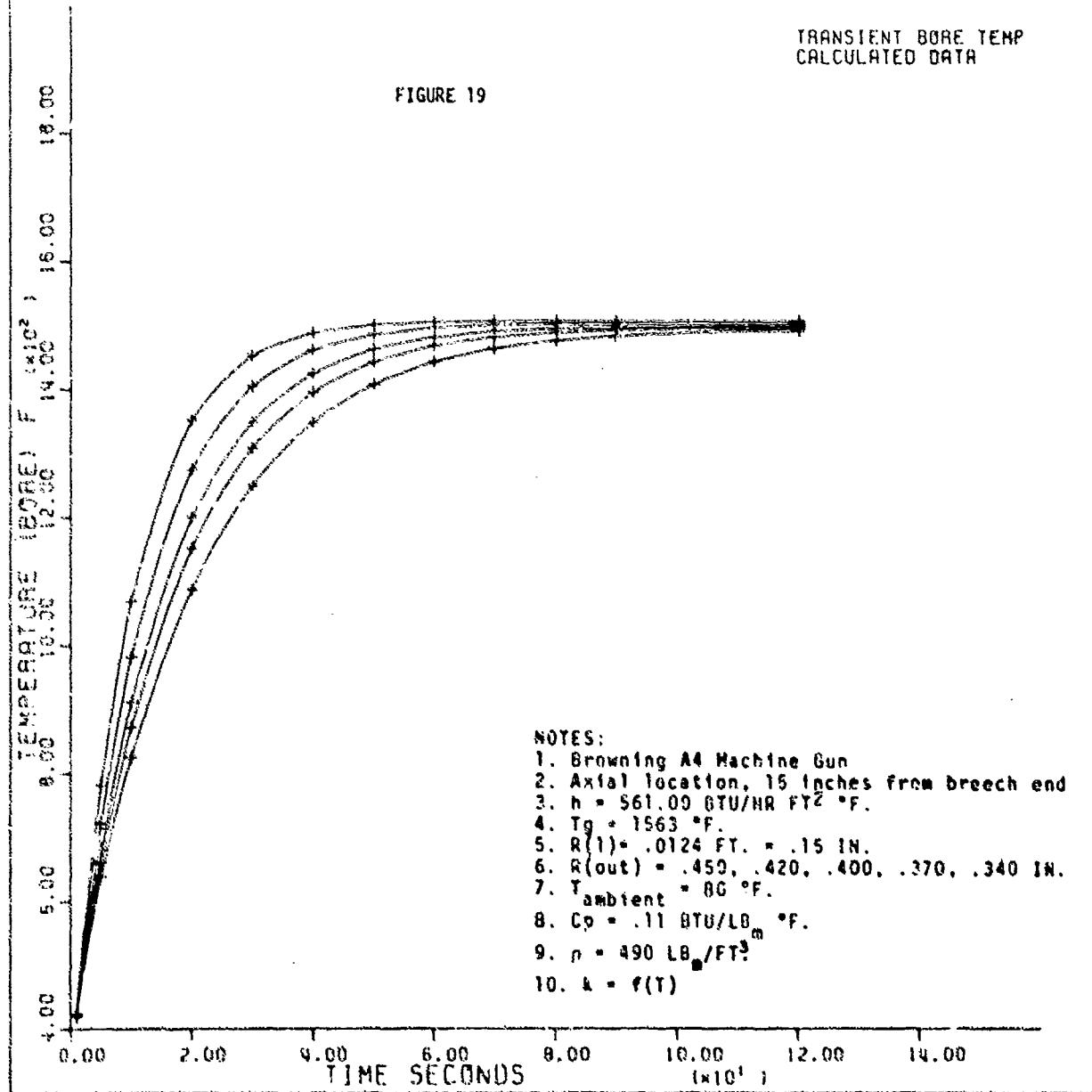
- NOTES:
1. Browning A4 Machine Gun
 2. Axial location, 9 inches from breech end
 3. $h = 421.00 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$
 4. $T_g = 1800 \text{ }^\circ\text{F}$
 5. $R(1) = .0124 \text{ FT} = .15 \text{ IN}$
 6. $R(\text{out}) = .450, .420, .400, .370, .340 \text{ IN}$
 7. $T_{\text{ambient}} = 80 \text{ }^\circ\text{F}$
 8. $C_p = .11 \text{ BTU/LB }^\circ\text{F}$
 9. $\rho = 490 \text{ LB}_m/\text{FT}^3$
 10. $k = f(T)$

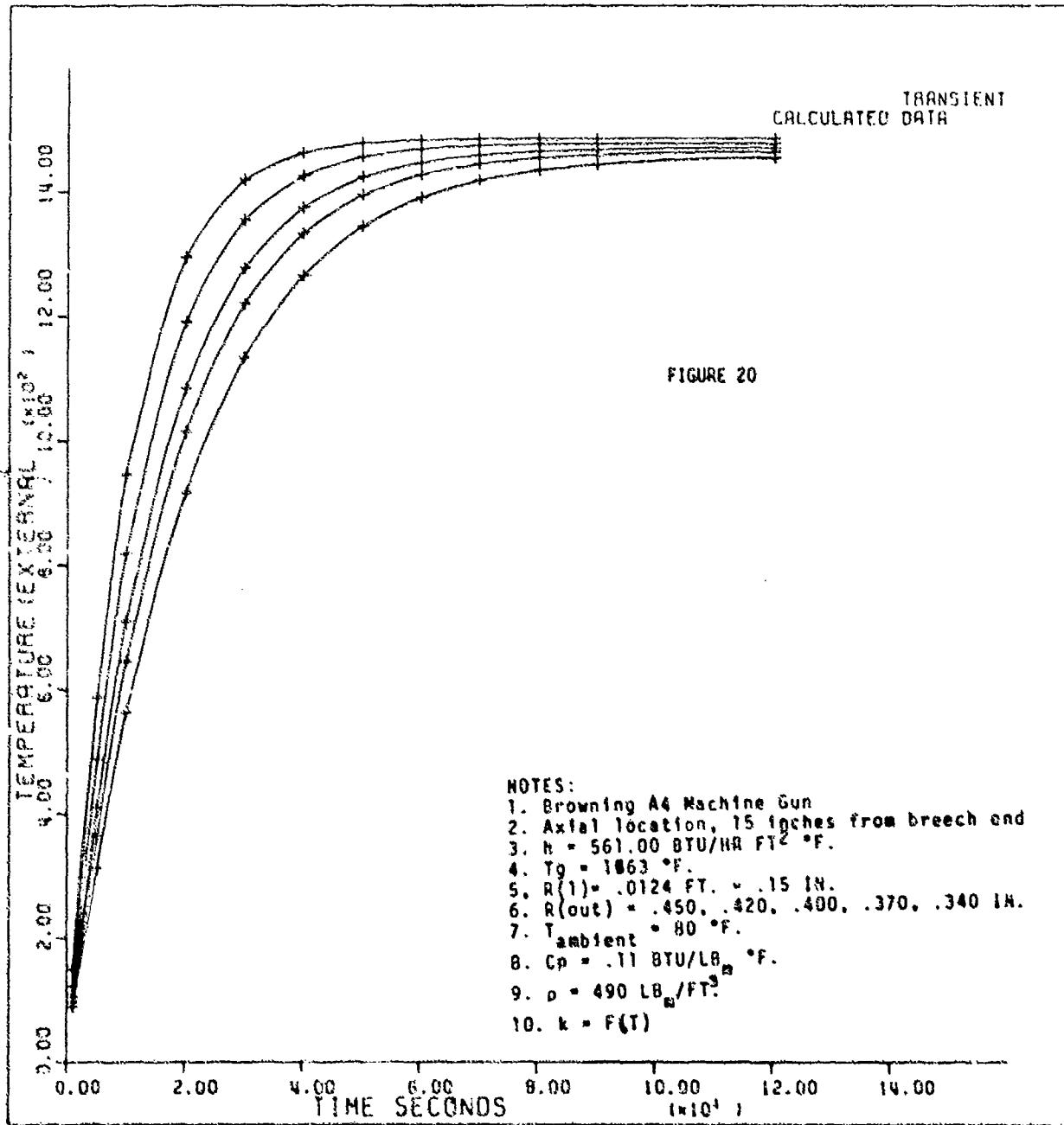




TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 19



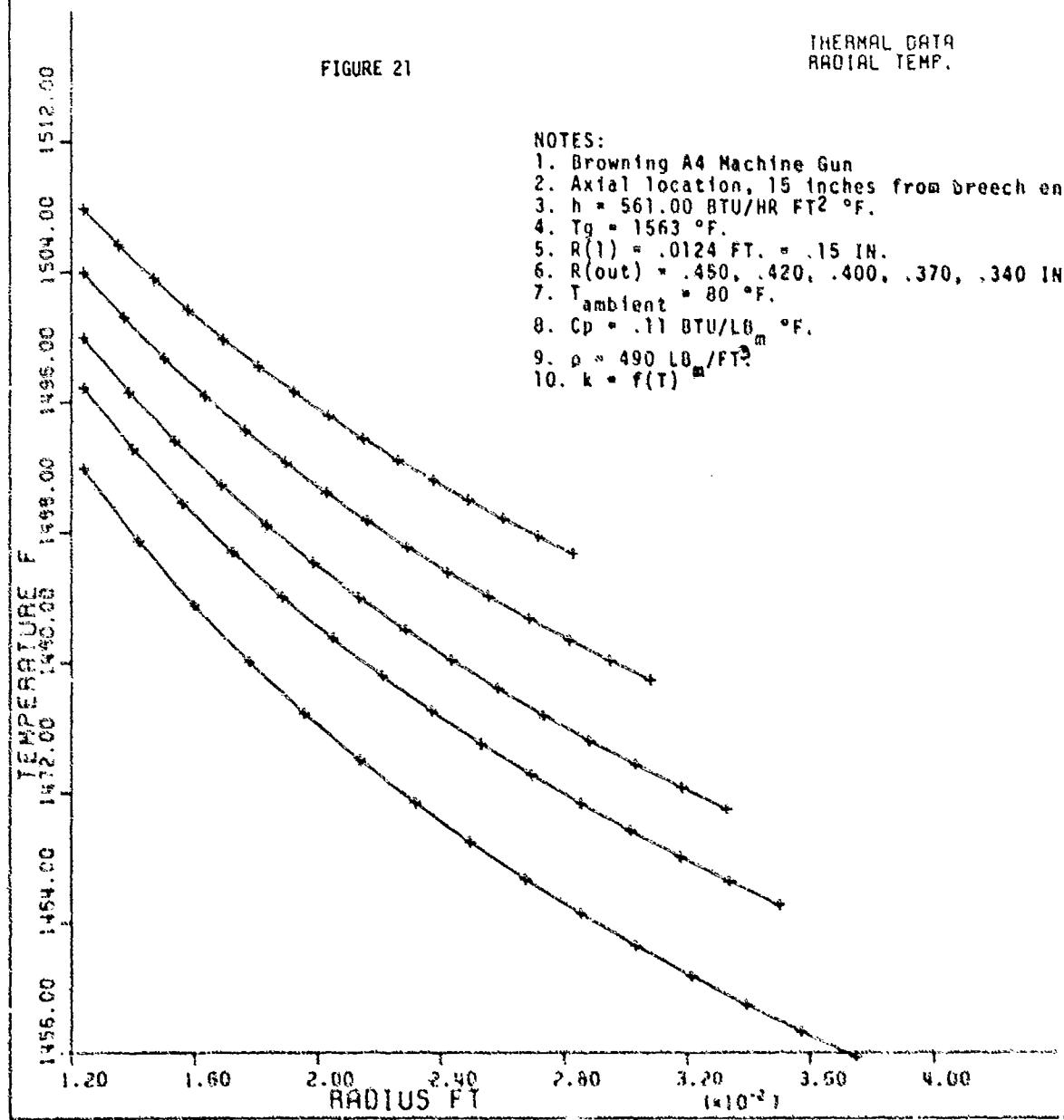


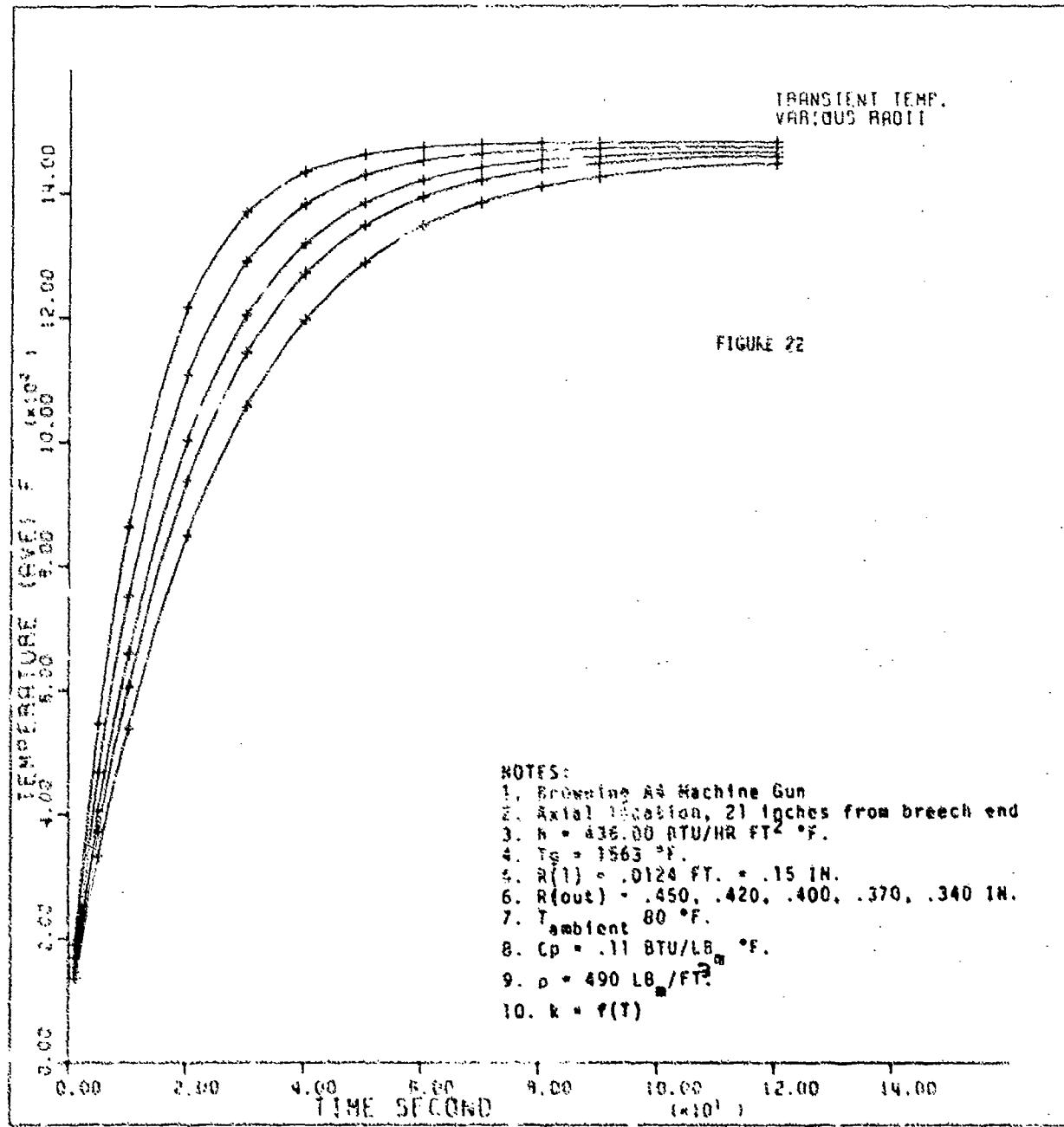
THERMAL DATA
RADIAL TEMP.

FIGURE 21

NOTES:

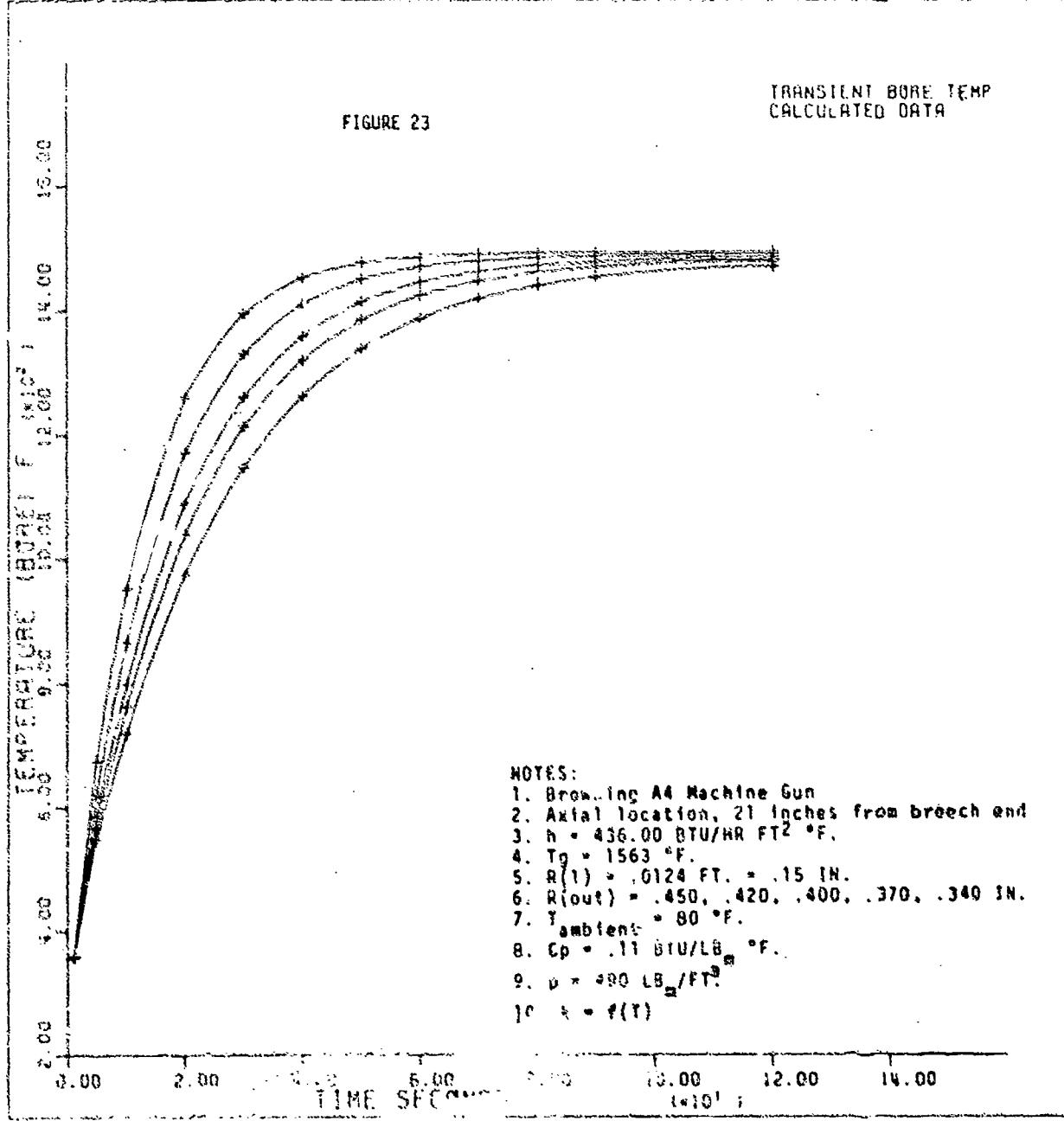
1. Browning A4 Machine Gun
2. Axial Location, 15 inches from breech end
3. $h = 561.00 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$.
4. $T_g = 1563 \text{ }^\circ\text{F}$.
5. $R(1) = .0124 \text{ FT.} = .15 \text{ IN.}$
6. $R(\text{out}) = .450, .420, .400, .370, .340 \text{ IN.}$
7. $T_{\text{ambient}} = 80 \text{ }^\circ\text{F.}$
8. $C_p = .11 \text{ BTU/LB}_m \text{ }^\circ\text{F.}$
9. $\rho = 490 \text{ LB}_m/\text{FT}^3$.
10. $k = f(T)$





TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 23



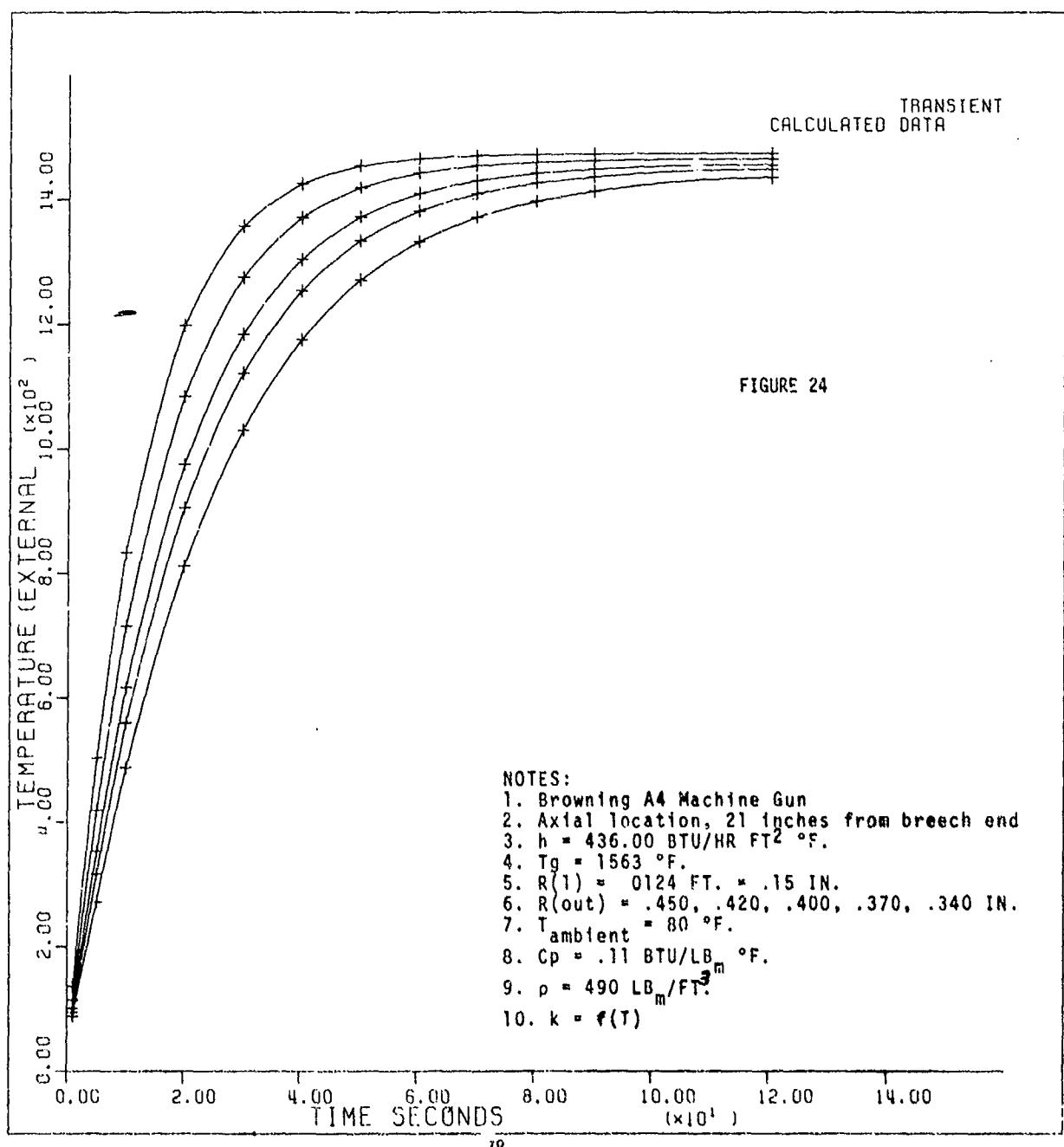


FIGURE 25

THERMAL DATA
RADIAL TEMP.

NOTES:

1. Browning A4 Machine Gun
2. Axial location, 21 inches from breech end
3. $h = 436.00 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$.
4. $T_g = 1563 \text{ }^\circ\text{F}$.
5. $R(1) = .0124 \text{ FT.} = .15 \text{ IN.}$
6. $R(\text{out}) = .450, .420, .400, .370, .340 \text{ IN.}$
7. $T_{\text{ambient}} = 80 \text{ }^\circ\text{F}$.
8. $C_p = .11 \text{ BTU/LB}_m \text{ }^\circ\text{F}$.
9. $\rho = 490 \text{ LB}_m/\text{FT}^3$.
10. $k = f(T)$

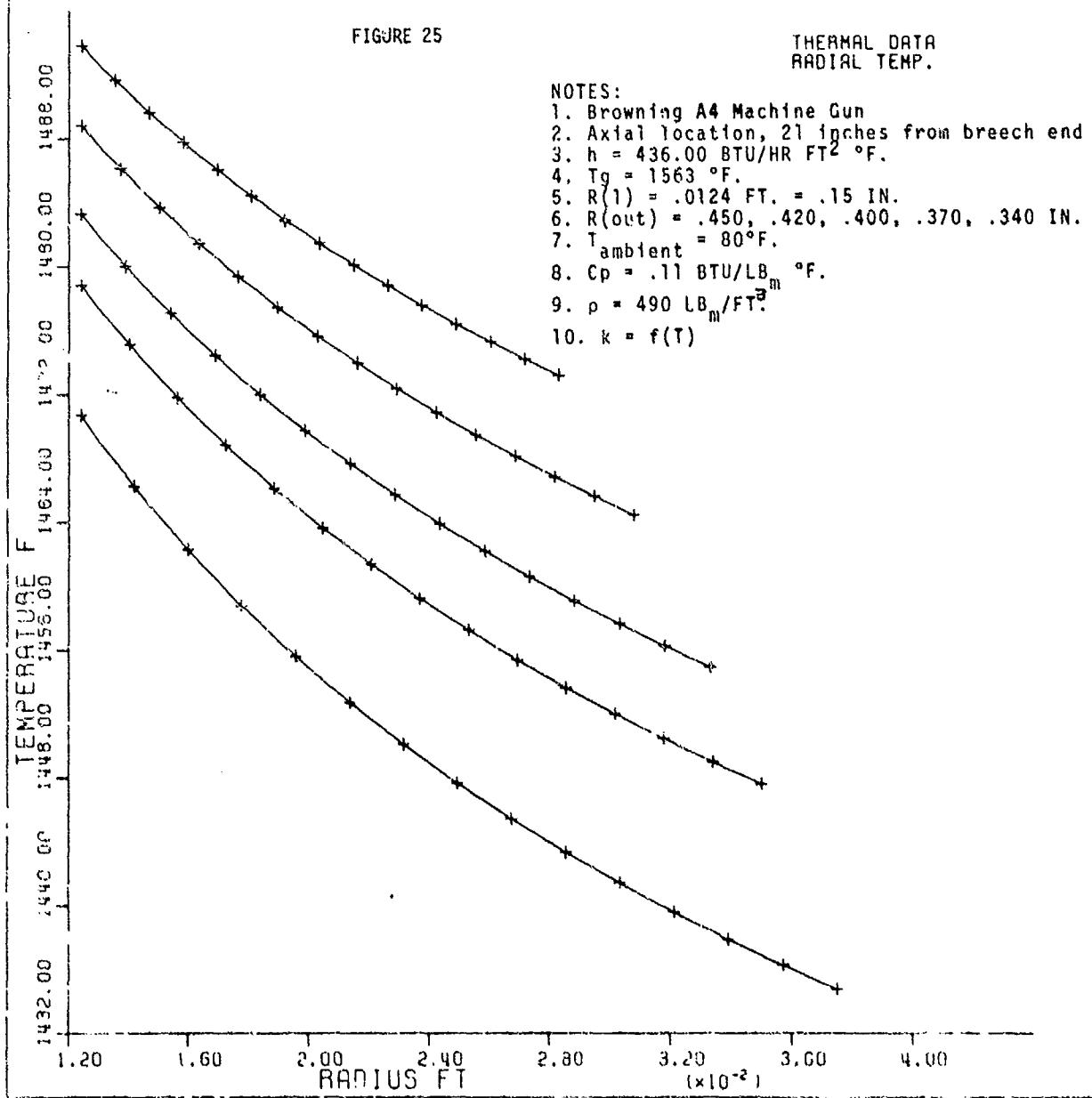
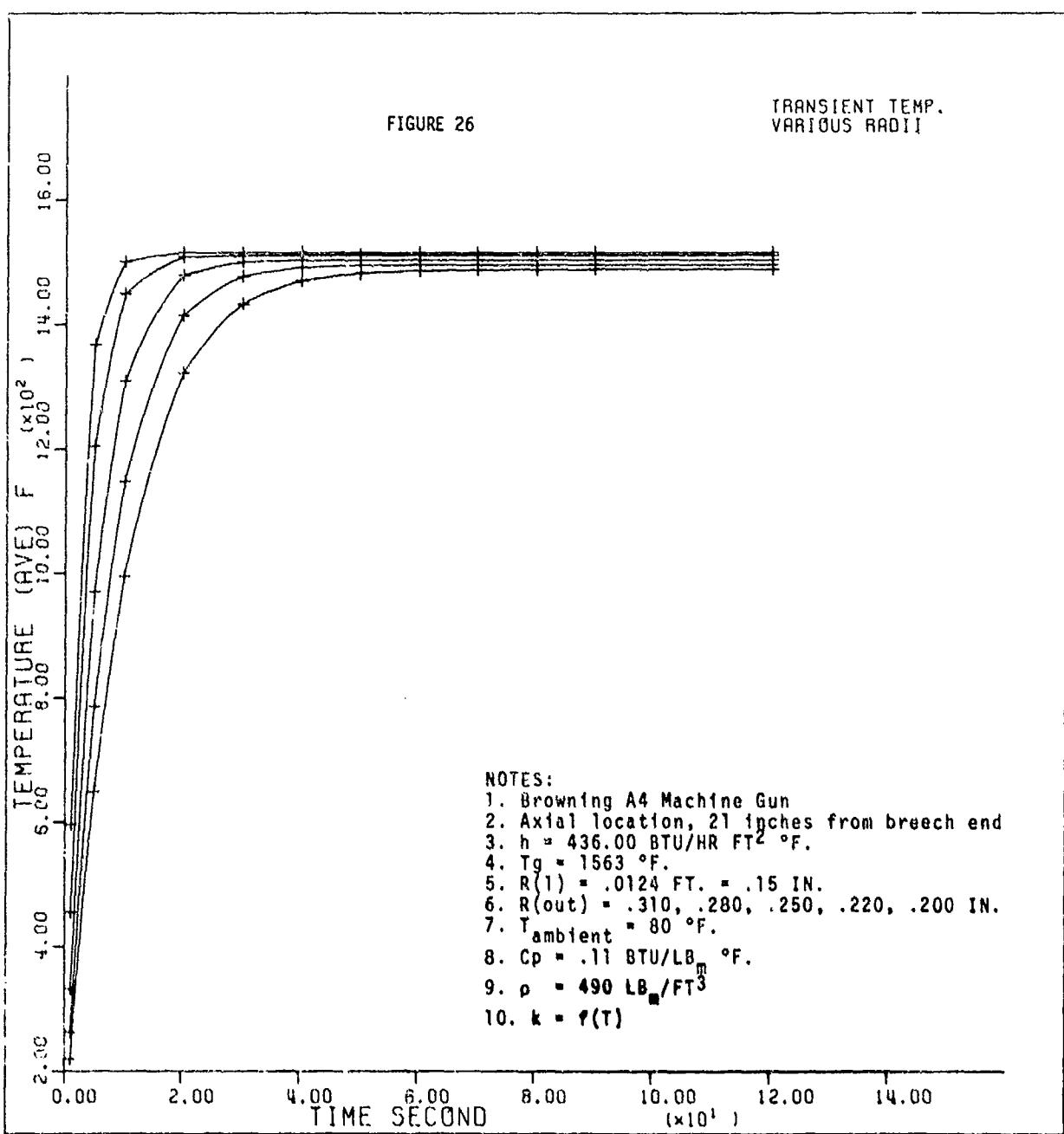
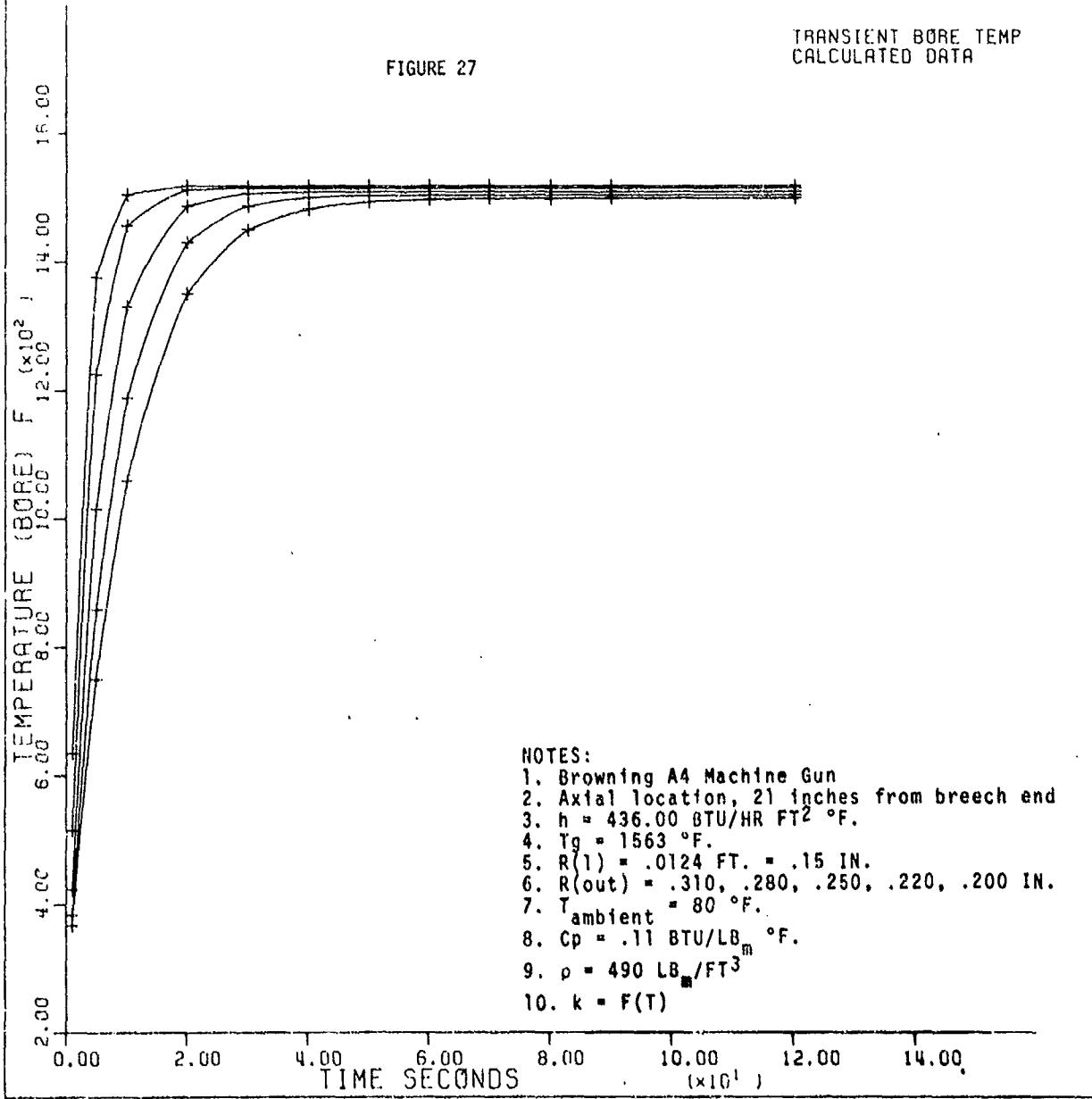


FIGURE 26

TRANSIENT TEMP.
VARIOUS RADII

TRANSIENT BORE TEMP
CALCULATED DATA

FIGURE 27



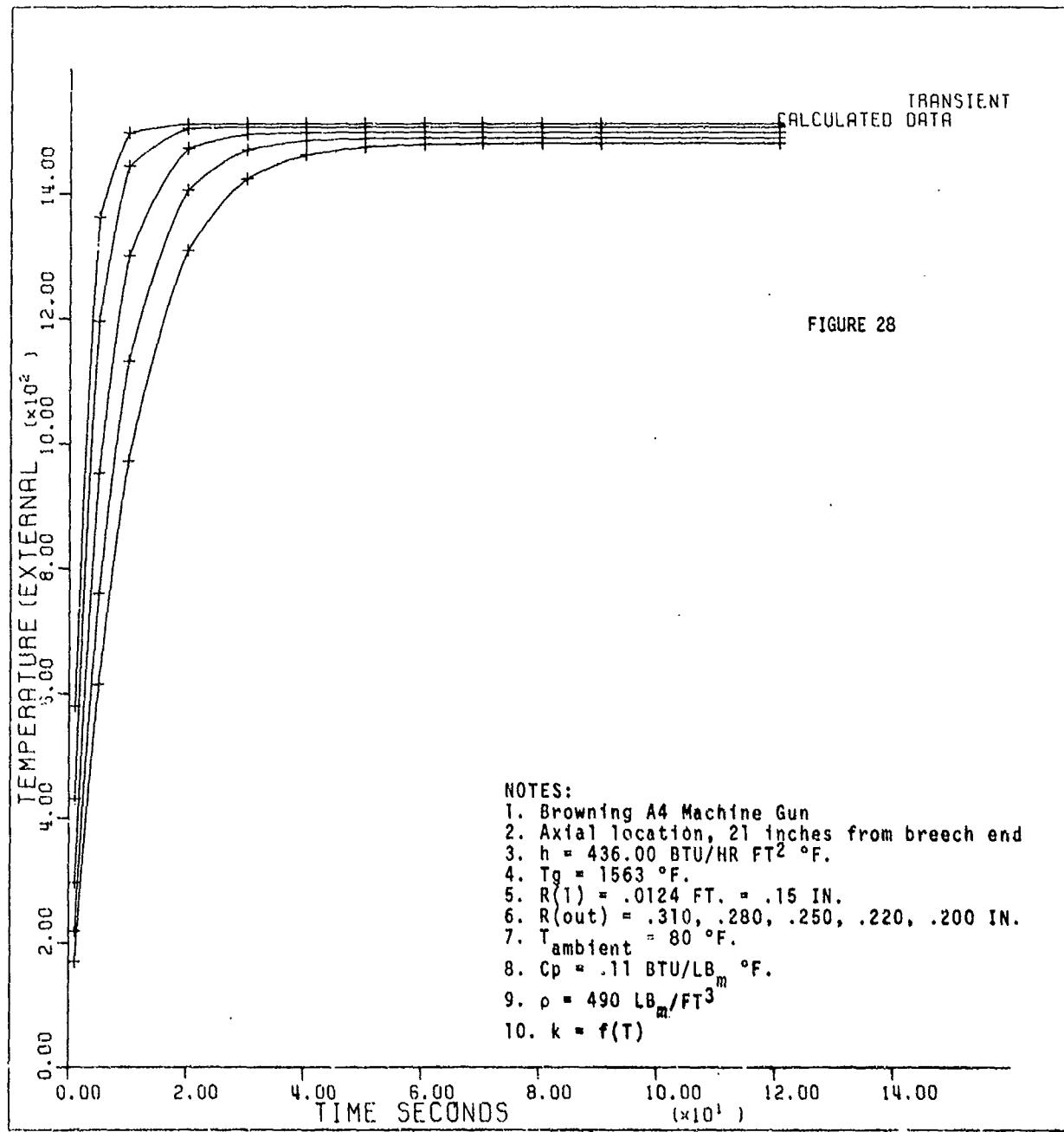
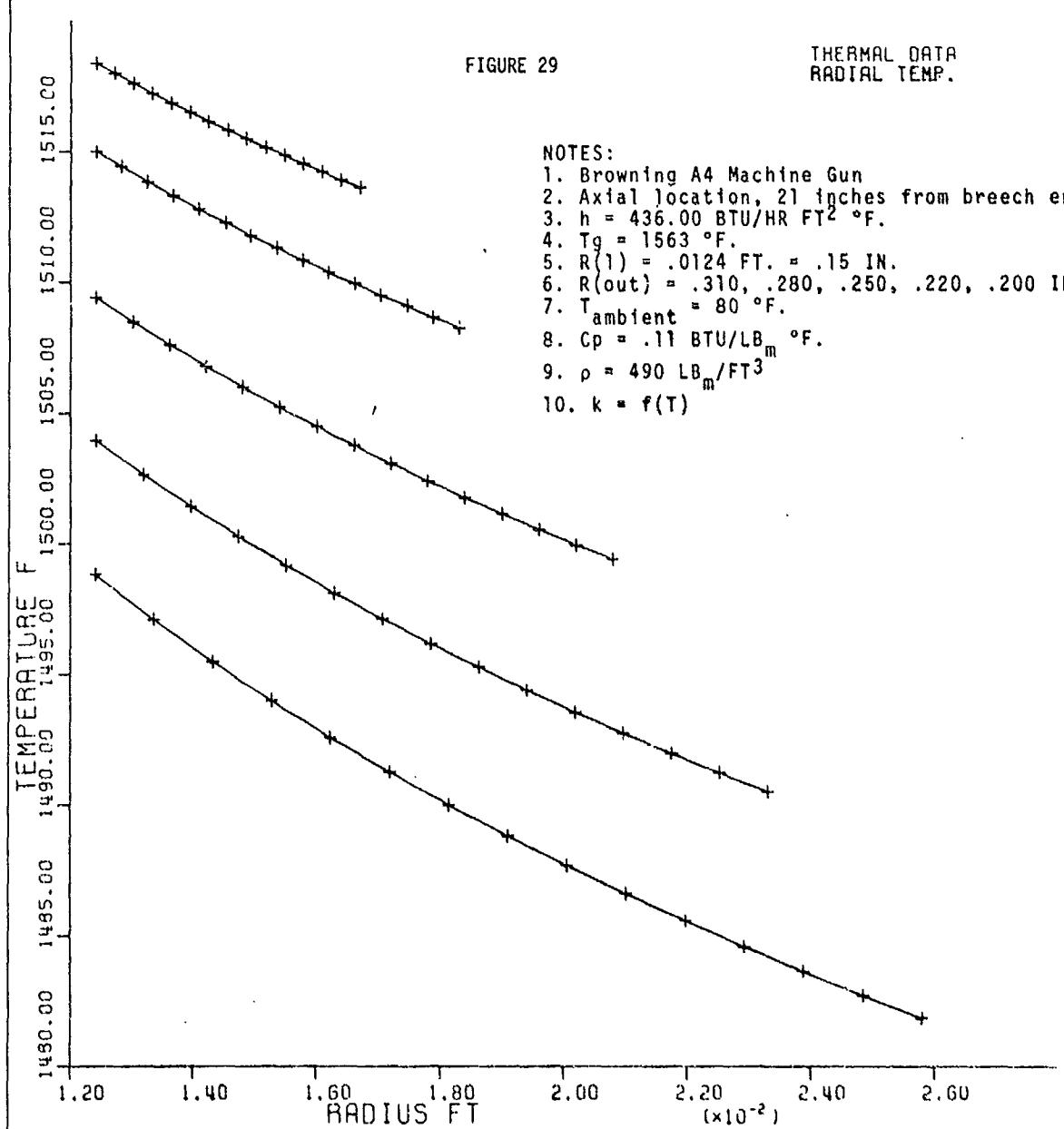


FIGURE 29

THERMAL DATA
RADIAL TEMP.

- NOTES:
1. Browning A4 Machine Gun
 2. Axial location, 21 inches from breech end
 3. $h = 436.00 \text{ BTU/HR FT}^2 \text{ }^\circ\text{F}$.
 4. $T_g = 1563 \text{ }^\circ\text{F}$.
 5. $R(1) = .0124 \text{ FT.} = .15 \text{ IN}$.
 6. $R(\text{out}) = .310, .280, .250, .220, .200 \text{ IN}$.
 7. $T_{\text{ambient}} = 80 \text{ }^\circ\text{F}$.
 8. $C_p = .11 \text{ BTU/LB}_m \text{ }^\circ\text{F}$.
 9. $\rho = 490 \text{ LB}_m/\text{FT}^3$
 10. $k = f(T)$



PROPOSED EXPERIMENTAL
30 CAL PROFILE

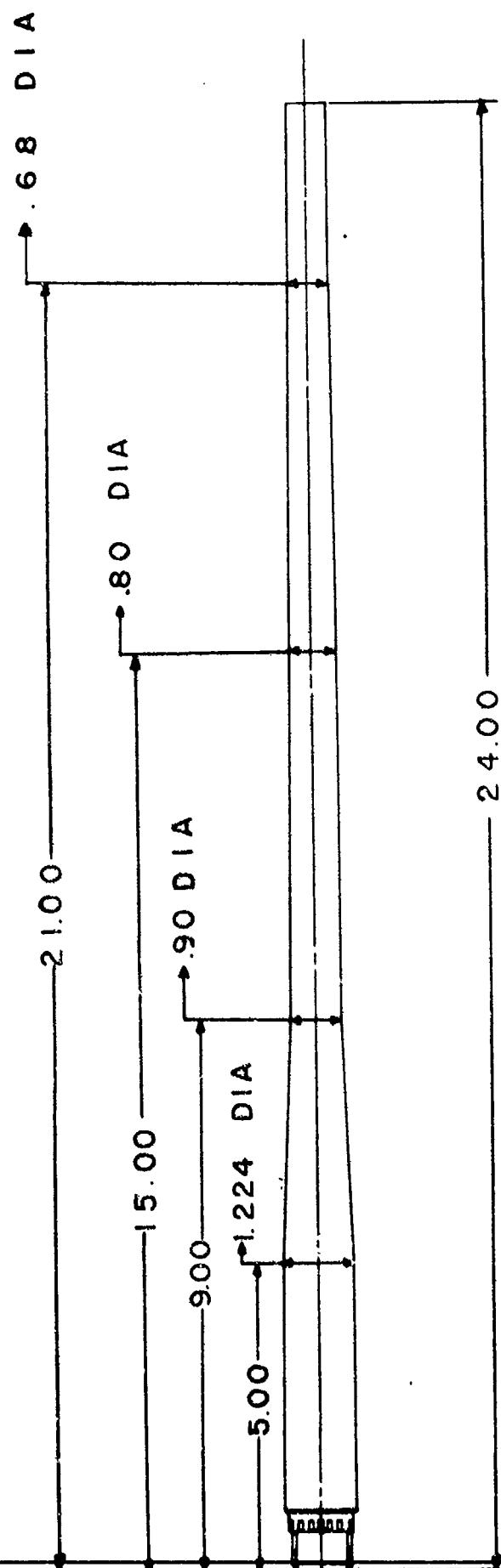


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Prepared by: Darrel M. Thomsen

Technical Report No.
 3 pages, Incl Figures & Tables

This report covers FY76 efforts on a project entitled "Effect of Material Mass Distribution on the Life of Small Arms Barrels." The objective of this project is to develop a semi-empirical technique for determining gun barrel wear (or erosion) as a function of barrel material properties, wall thickness (or ratio) and firing rate. The past years task involved analytical design of test specimens (barrel geometries) for firing experiments wherein regression analyses will be performed in the determination of the effect of mass distribution on barrel life. A useful design tool (cont.) over

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